



Allothermal gasification of biomass into chemicals and secondary energy carriers

Presented at International Conference on Polygeneration Strategies (ICPS09)
1-4 September 2009 in Wien, Austria.

R.W.R. Zwart

Allothermal gasification of biomass into chemicals and secondary energy carriers

Robin Zwart



Motivation for polygeneration

Make more
money
out of wood



↑
High value product!

Increase the
efficiency of
wood conversion

Motivation for polygeneration



↑
Sales benefits?

↑
High value product!

↑
Production costs?

Outline allothermal gasification towards chemicals and secondary energy carriers

- Motivation for polygeneration

- Allothermal gasification: the MILENA at ECN
- Primary gas cleaning: the OLGA for tar removal

- Possible secondary energy carriers
- Possible chemicals

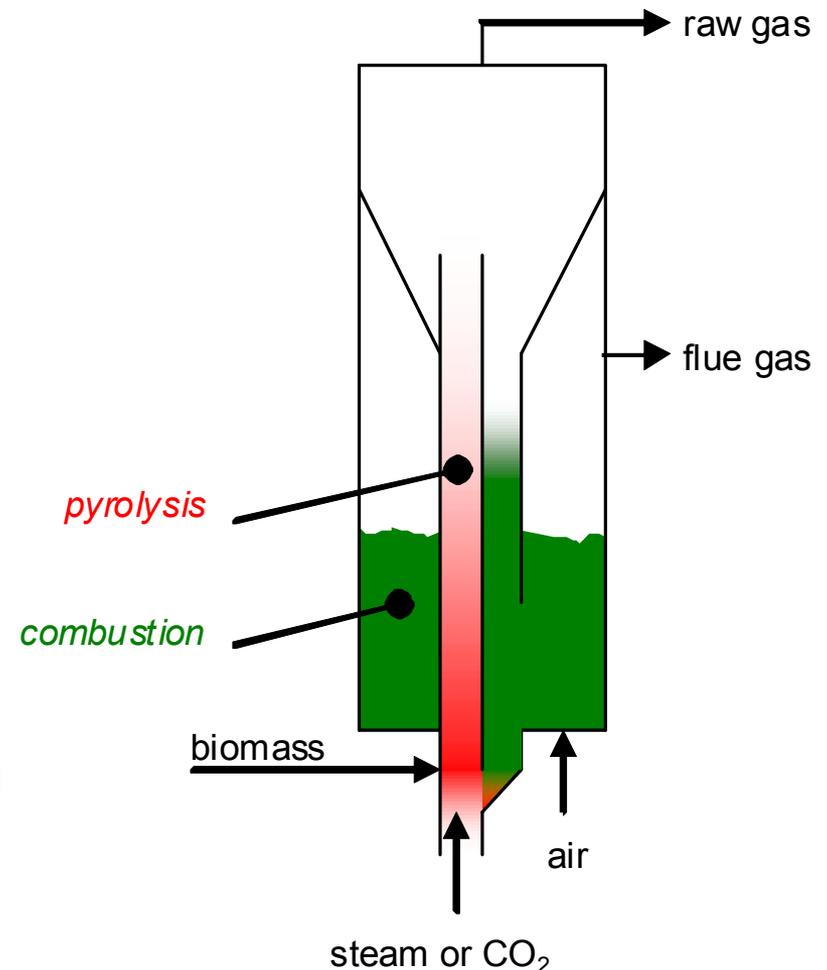
- Polygeneration concept and its feasibility

Allothermal gasification: MILENA at ECN

- Low N₂ in gas
- High methane yield
- Complete conversion
- Fuel flexible

160 kg/hr pilot plant:

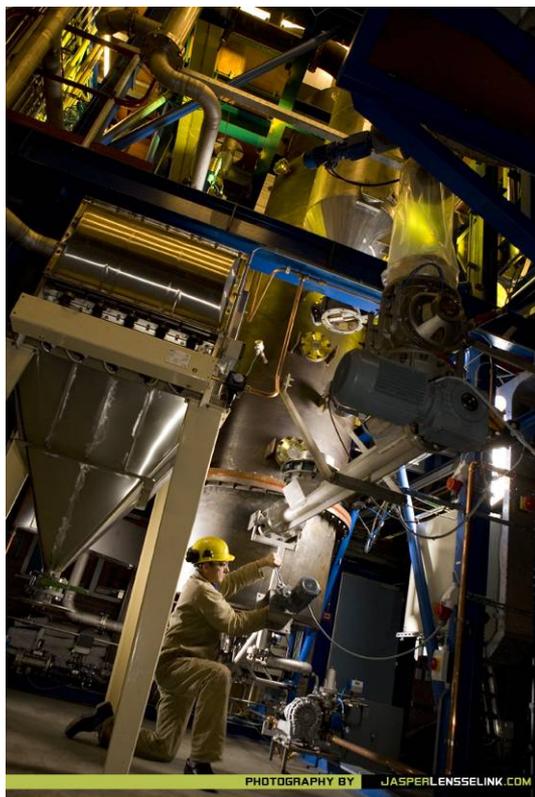
- Riser diameter 0.2 m
- Combustor diameter 0.8 m
- Height 8.0 m



Allothermal gasification: MILENA at ECN



25 kW



800 kW



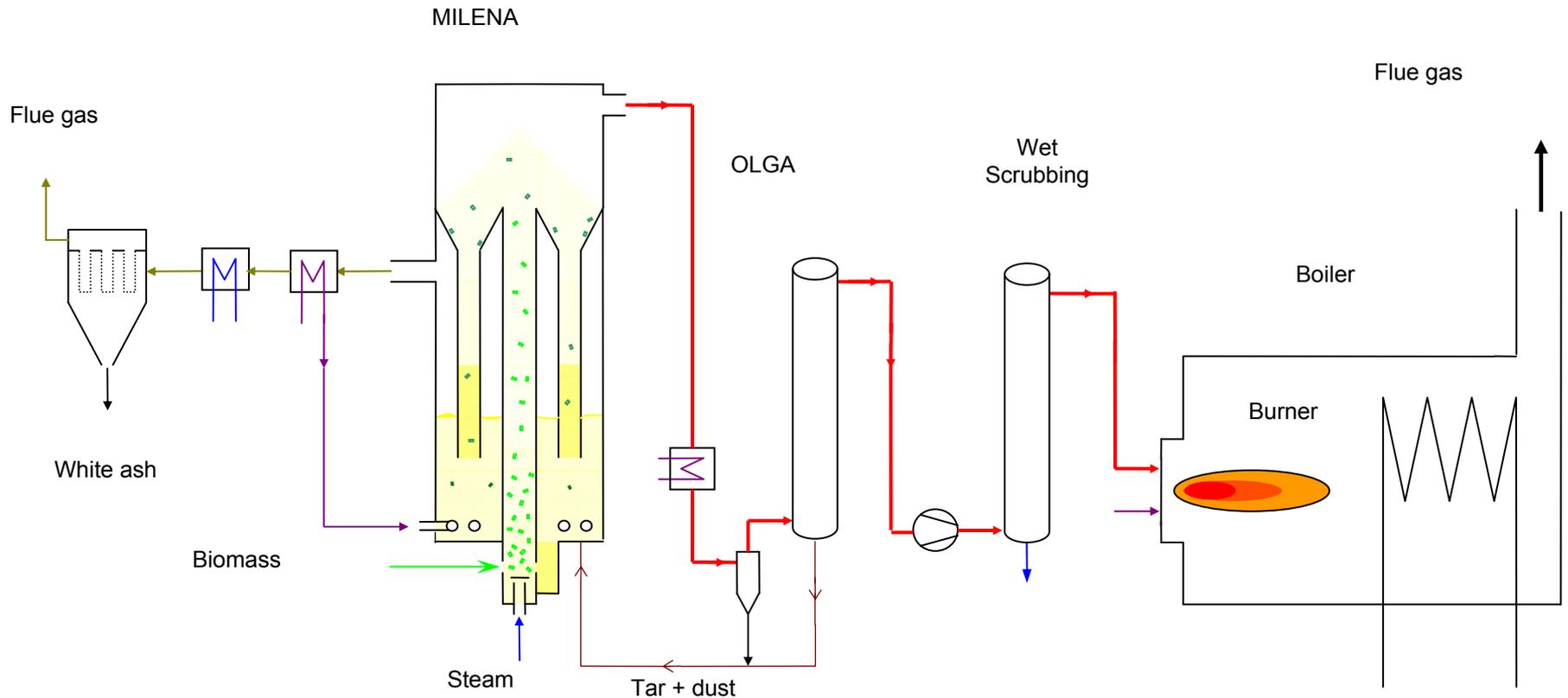
CHP
10 MWth

scheduled for
2012

SNG
50 MWth

scheduled for
2015

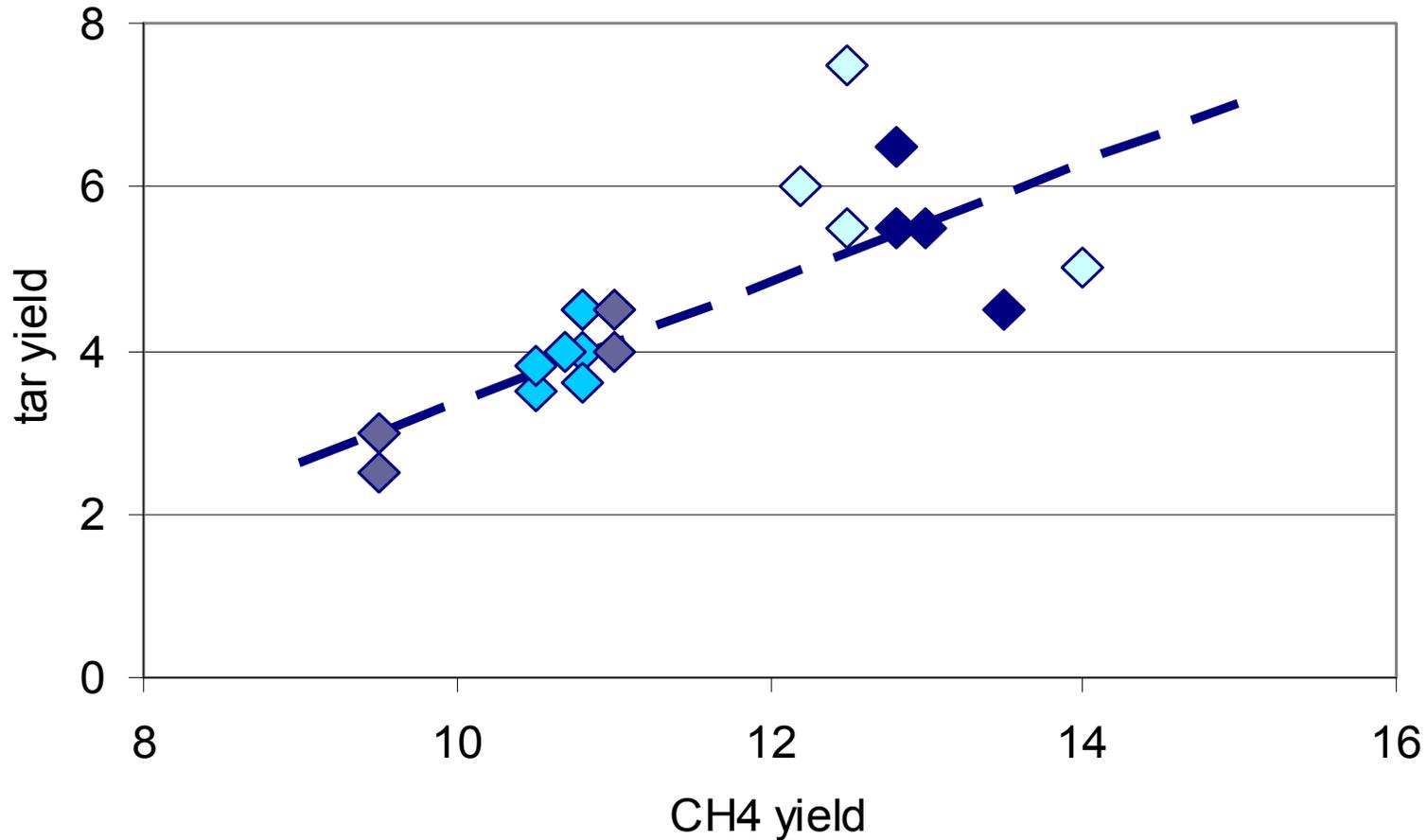
Allothermal gasification: MILENA at ECN



Allothermal gasification: MILENA at ECN

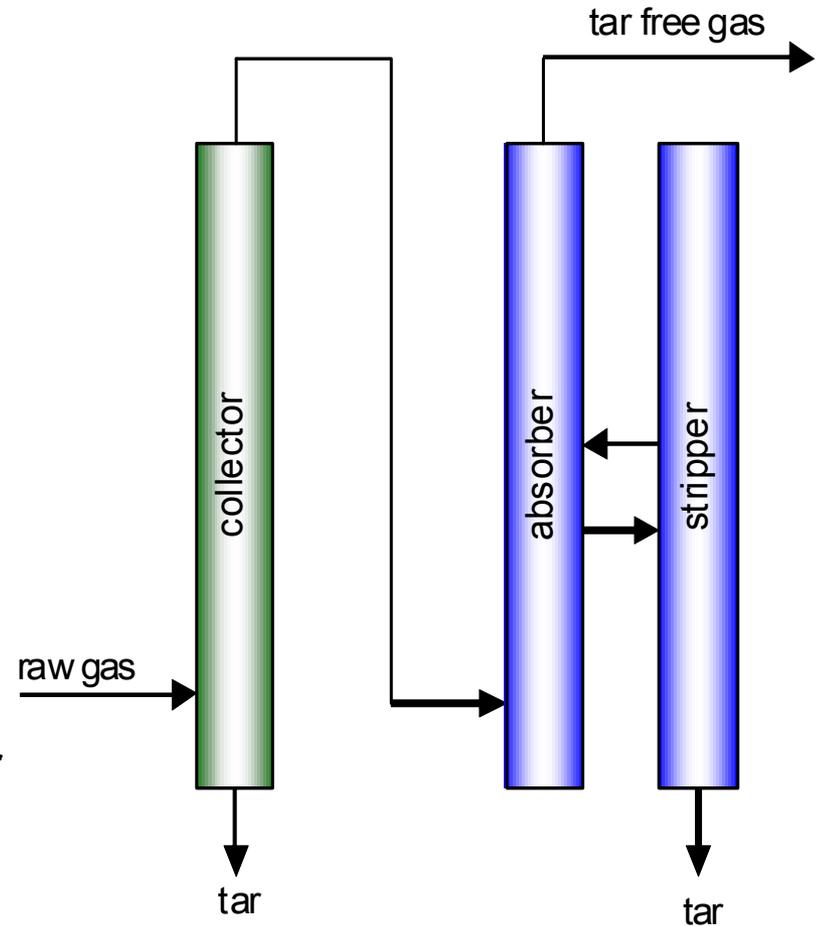
- Approximately 15 tests done, initially directly to the boiler.
- Fuel: wood pellets, throughput 120 and 150 kg/h
- Fluidization agent gasifier: steam (15 kg/h) or air (20 m_n³/h)
- Bed material -> Sand
- Estimated circulation rate bed material 3000 kg/h (design 6000). Circulation rate can be increased during testing
- Gas composition similar to lab-scale installation (tar content approx. 40 gram/m_n³)
- Issues to be solved:
 - Tar removal required (OLGA), tar condensation in front of burner, OLGA will be ready in **August**.
 - Sand causes friction problems between refractory wall and metal insert, modifications required.

Allothermal gasification: MILENA at ECN



Primary gas cleaning: OLGA for tar removal

- Complete tar removal
 - No methane reduction
 - Tar recycle to gasifier
 - No water condensation
 - Fits many types of gasifiers
-
- Creates freedom for gasifier optimization ...

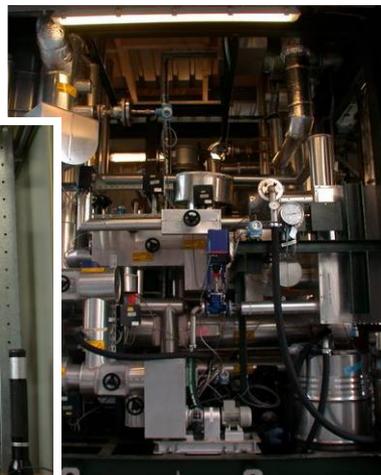


Primary gas cleaning: OLGA for tar removal

DAHLMAN
FILTER TECHNOLOGY



$2 \text{ m}^3/\text{h}$



$200 \text{ m}^3/\text{h}$



$2\ 000 \text{ m}^3/\text{h}$



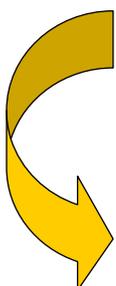
$25\ 000 \text{ m}^3/\text{h}$

Primary gas cleaning: OLGA for tar removal

Component		Downstream MILENA	Downstream OLGA
CO	vol%	30.1	30.6
H2	vol%	32.0	32.5
CO2	vol%	19.2	19.4
O2	vol%	0.0	0.0
CH4	vol%	12.2	12.4
N2+Ar	vol%	0.1	0.1
C2H2	vol%	0.2	0.2
C2H4	vol%	3.9	3.9
C2H6	vol%	0.2	0.2
C6H6	vol%	1.0	0.5
C7H8	vol%	0.1	0.0
Tar	g/mn3	52.1	0.2

Possible secondary energy carriers

- Standard quality substitute natural gas (CH_4)
 - High quality substitute natural gas (CH_4 , C_2H_6 , ...)
-
- C1 chemistry based fuels ($\text{CO} + \text{H}_2 \rightarrow \text{FT diesel, DME, ...}$)
 - “The ultimate fuel” (H_2)
-
- Heat
 - Power



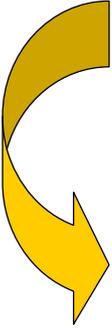
All will depend on the scale of operation!

Possible chemicals

- Acetylene (C_2H_2 for bulk chemistry)
- Ethylene (C_2H_4 for bulk chemistry)

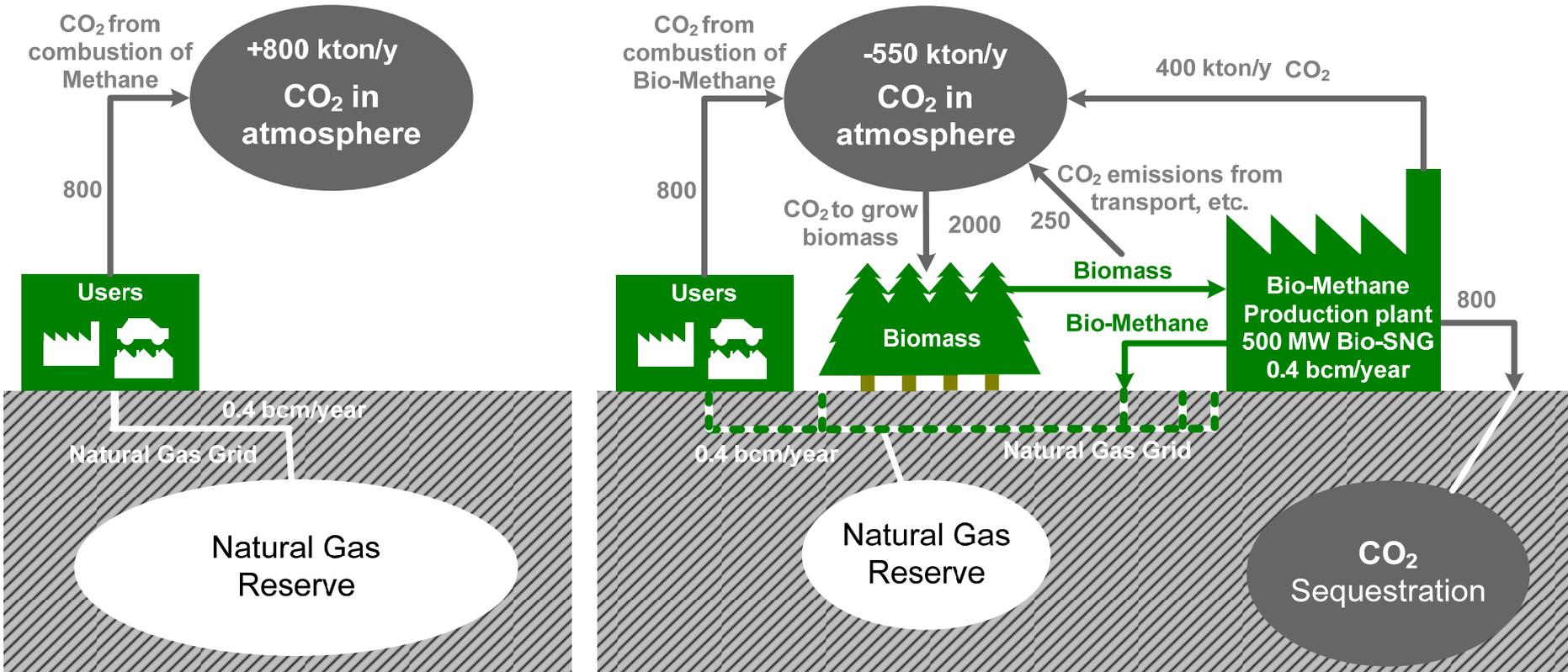
- Benzene (C_6H_6 for bulk chemistry)
- Toluene (C_7H_8 for bulk chemistry)

- Carbon dioxide (CO_2 for greenhouses)

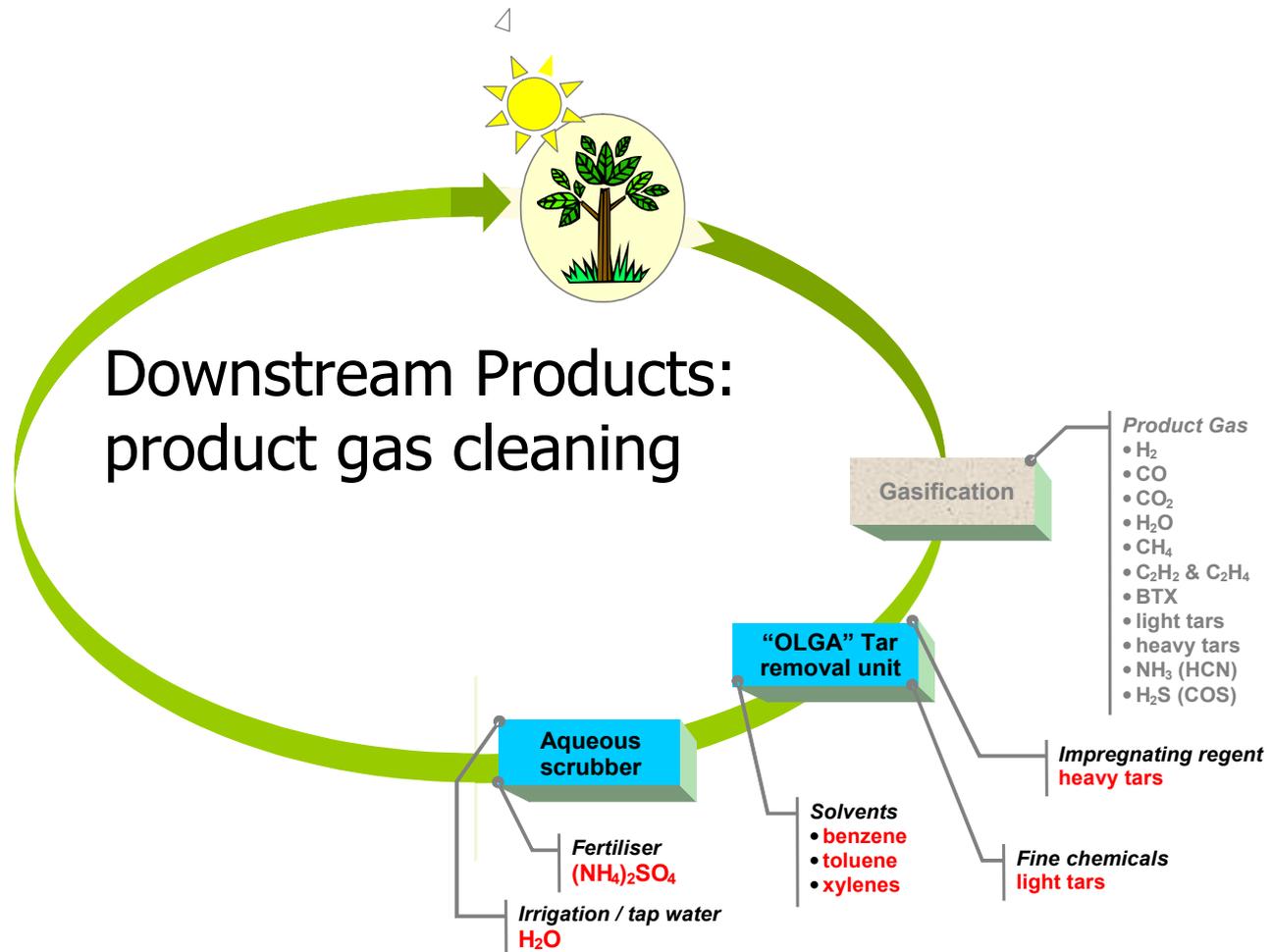


In many systems including a synthesis step, CO_2 removal is implemented for volume reduction or product quality control!

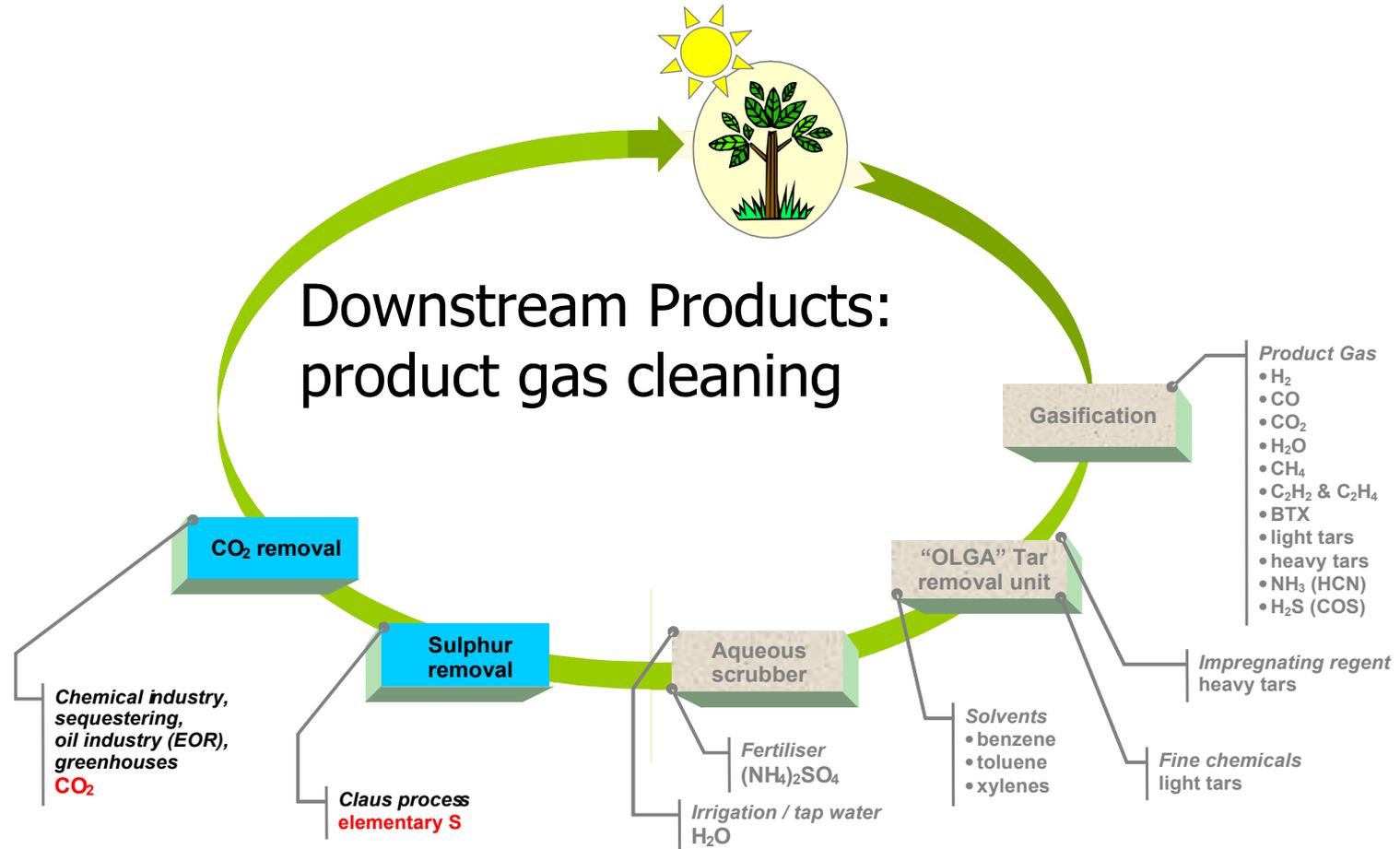
Possible chemicals



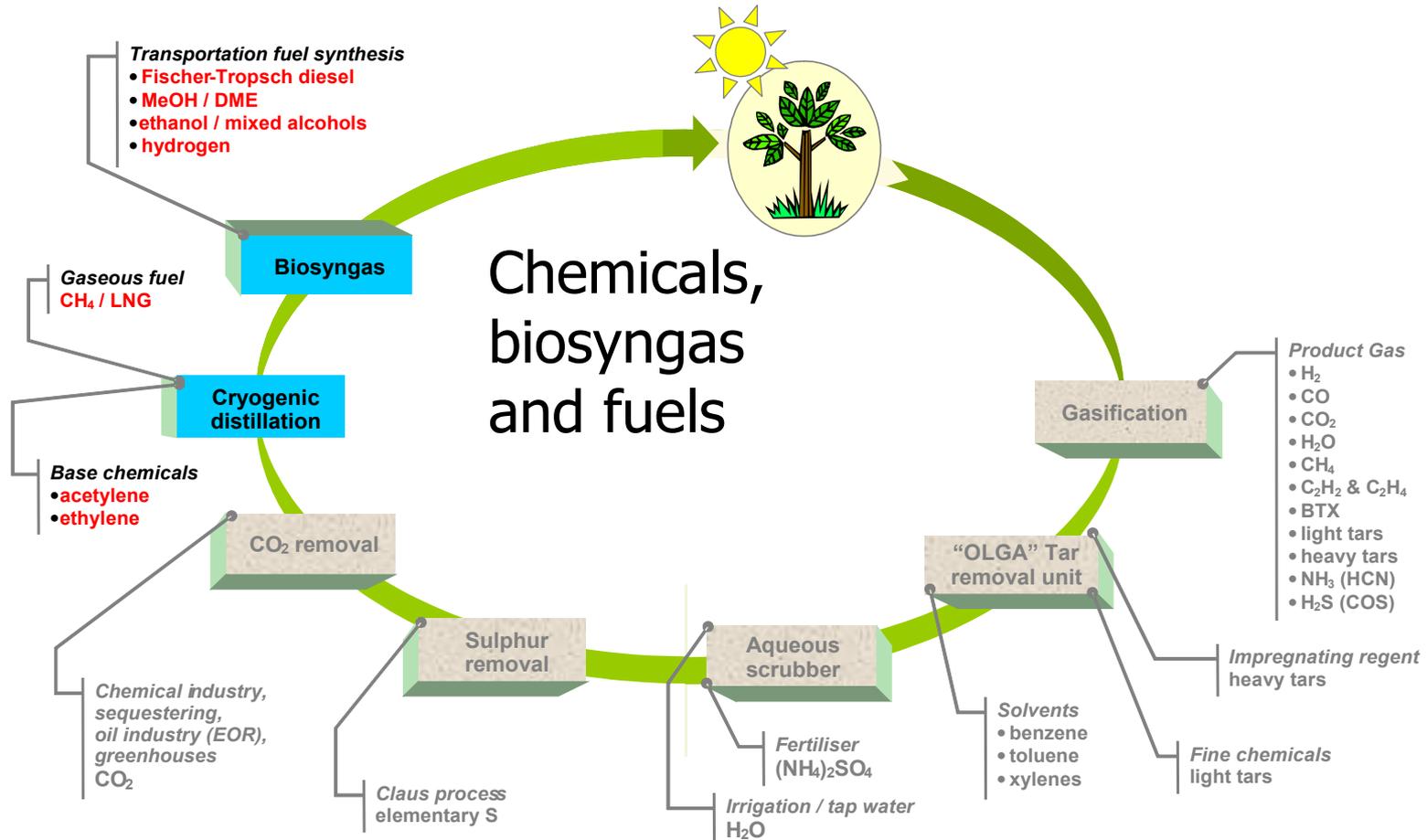
Polygeneration concept



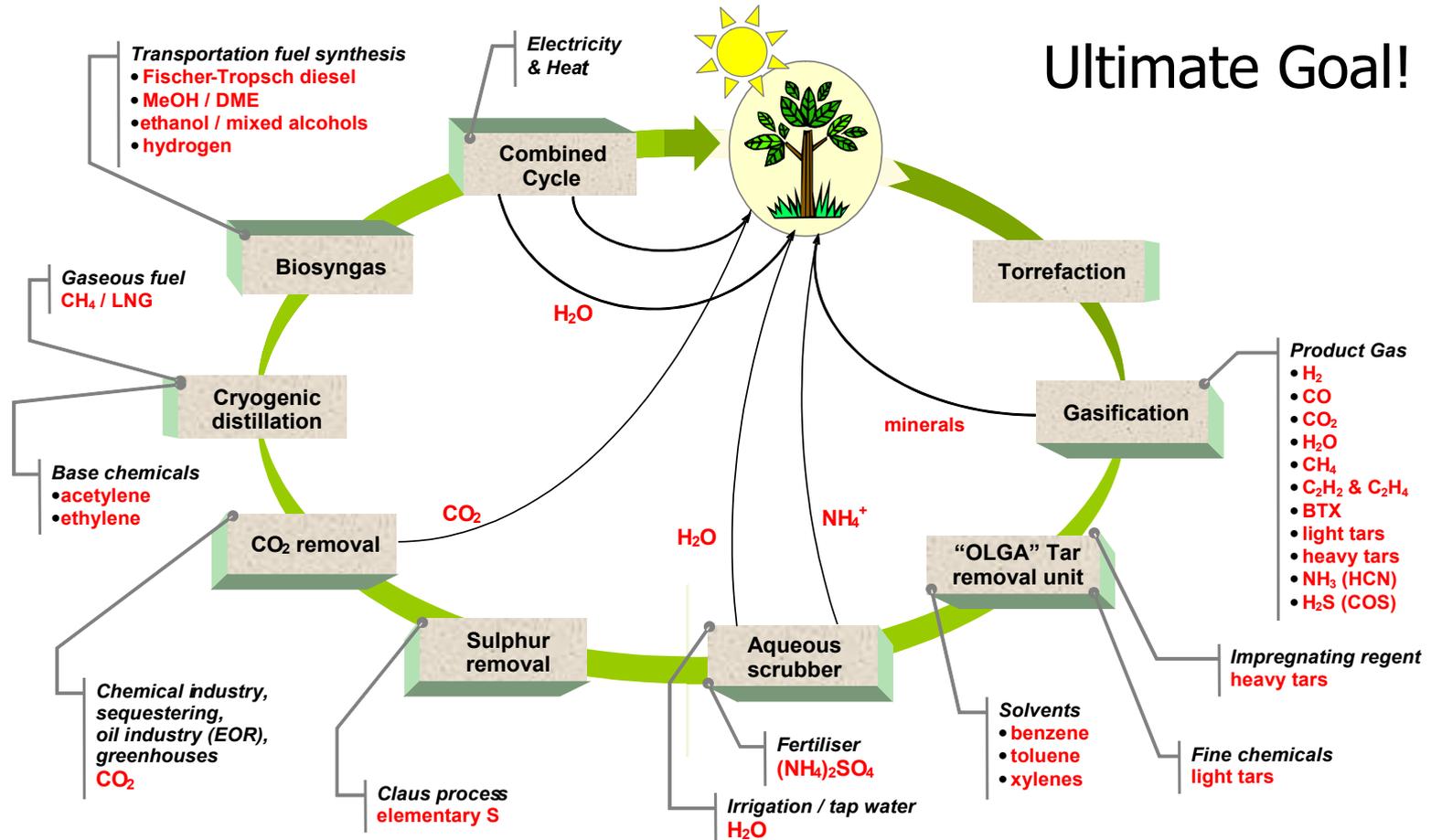
Polygeneration concept



Polygeneration concept

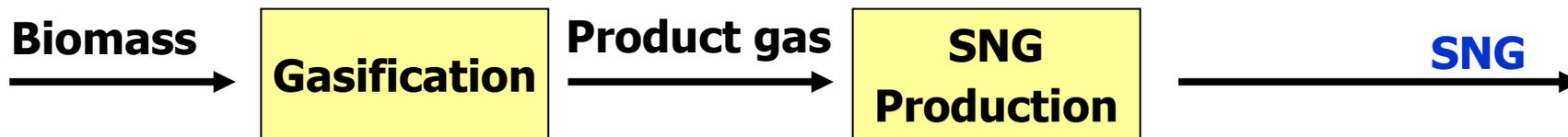


Polygeneration concept

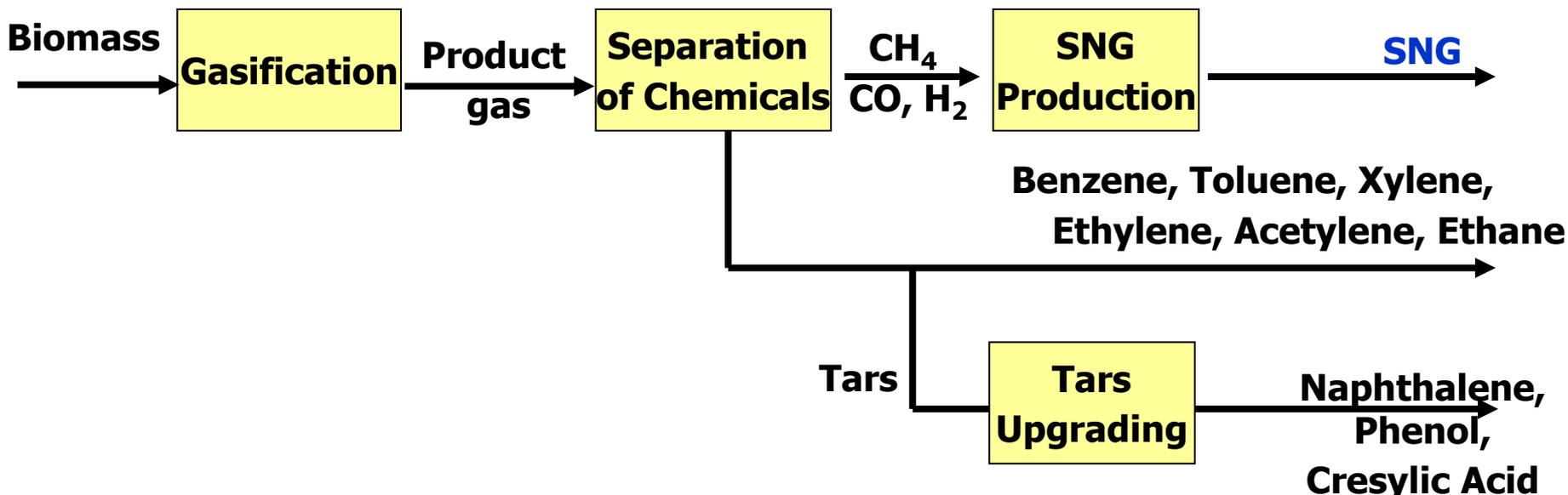


Feasibility

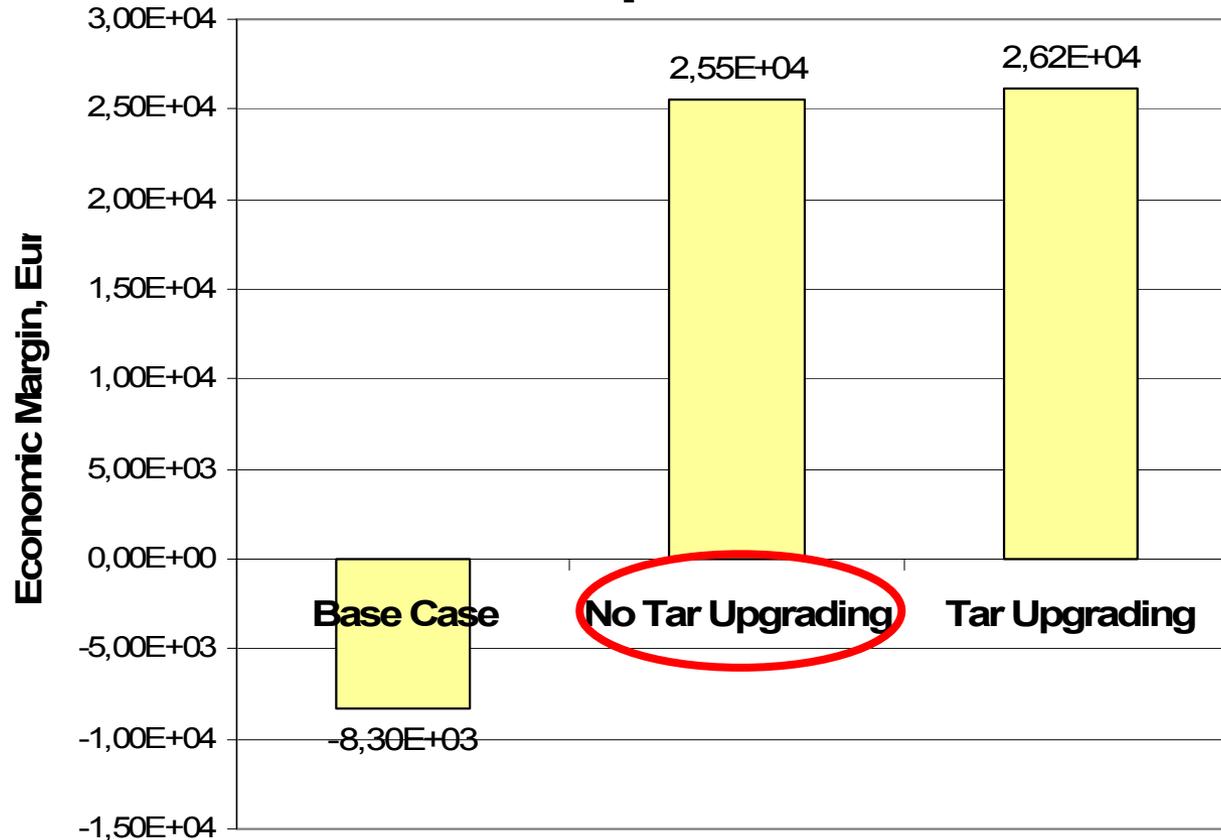
1. Base Case : SNG Production via low temperature gasification



2. Separation of Chemicals



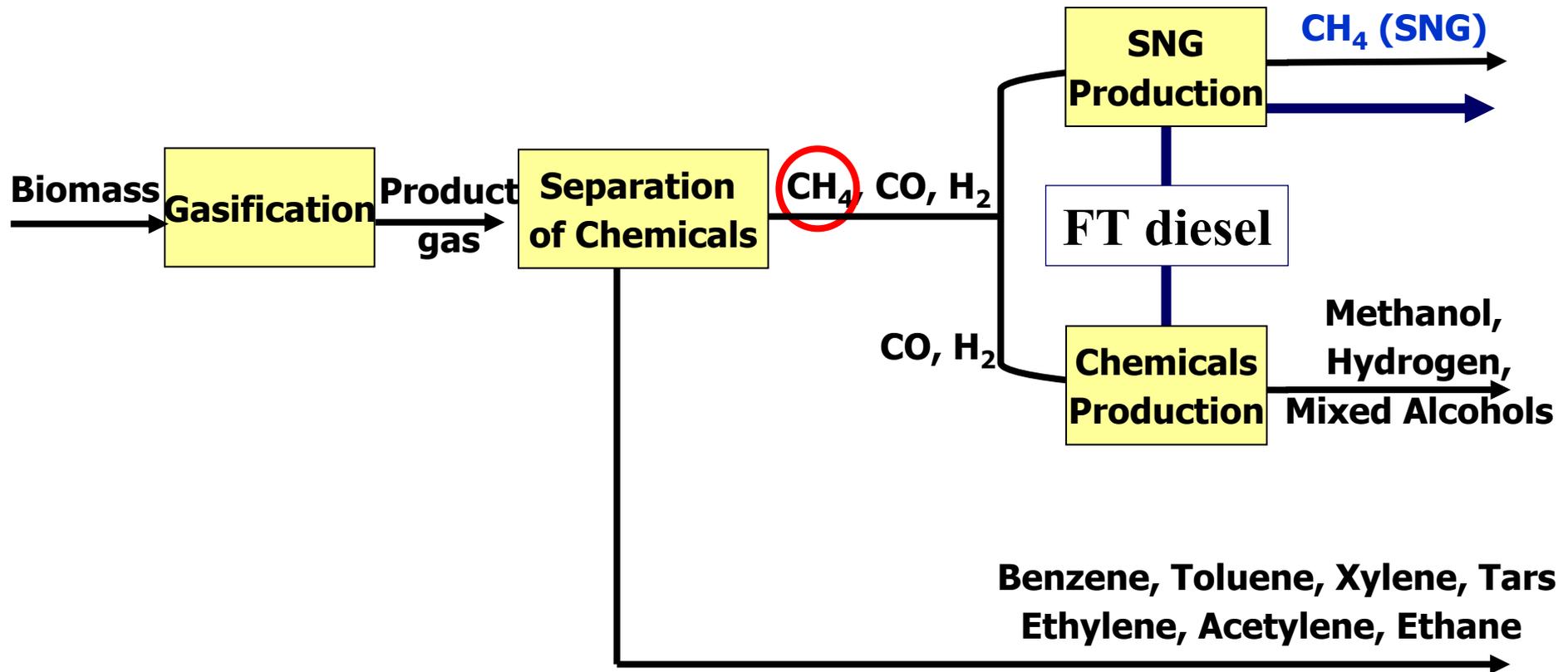
Feasibility Comparison



Economic Margin = Sales Revenues – Raw Materials (Biomass)
 (on the basis of 100 kg/hr input of biomass)

Feasibility

3. Separation of Chemicals and Catalytic production of Chemicals



Feasibility

592 *Energy & Fuels*, Vol. 19, No. 2, 2005

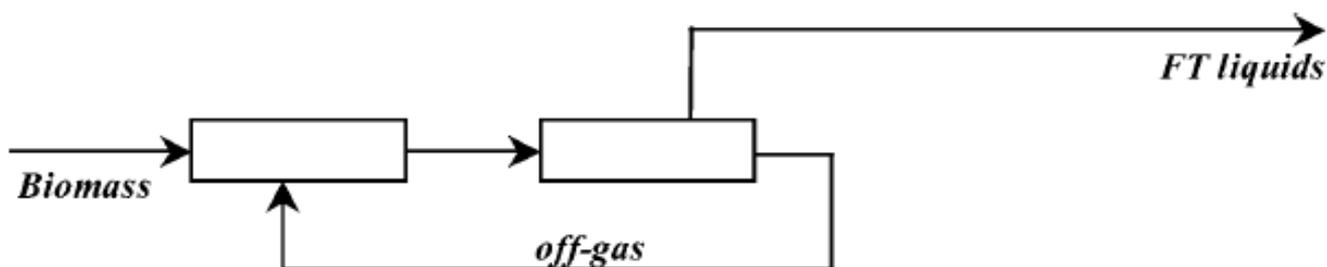


Figure 1. System for the production of Fischer–Tropsch (FT) liquids from biomass.

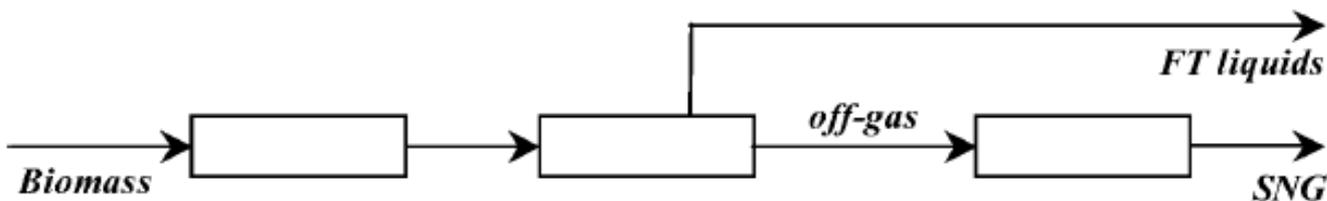
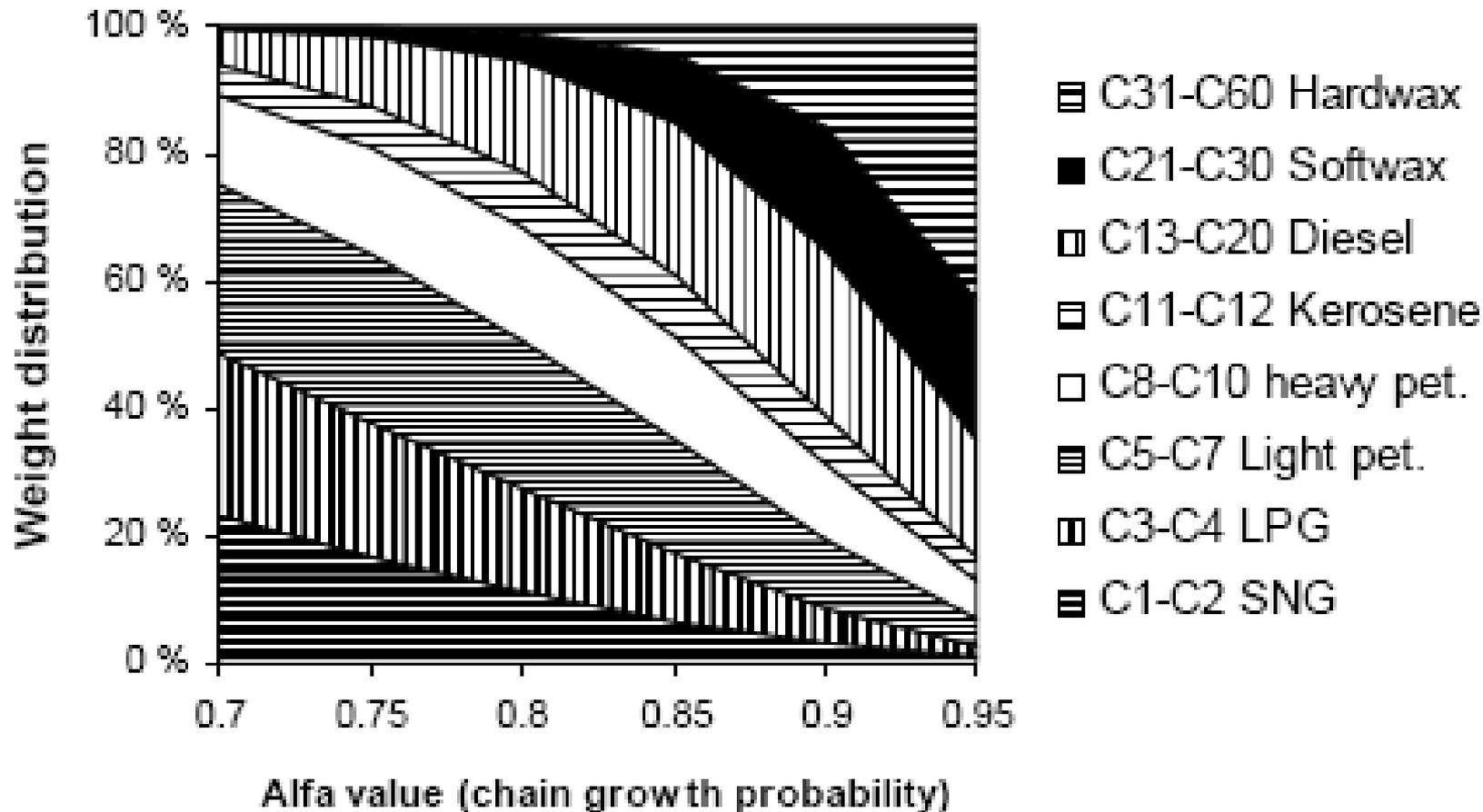


Figure 2. System for the co-generation of liquid FT transportation fuels and synthetic natural gas (SNG) from biomass.

Feasibility



Conclusion

- Polygeneration can be more than co-producing heat/power
- Chemicals can create additional economic margin...
... though will require significant additional costs
- Fuels can create additional economic margin...
... and might require less additional costs than thought
- Why work on allothermal gasification and C1 chemistry...
... when your product gas contains all the interesting stuff?

Contact information

Robin Zwart

e: zwart@ecn.nl

t: +31 224 56 4574

w: www.ecn.nl

PO Box 1

NL 1755 ZG Petten

the Netherlands

publications: www.ecn.nl/publications

fuel composition database: www.phyllis.nl

tar dew point calculator: www.thersites.nl

IEA bioenergy/gasification: www.ieatask33.org

Milena indirect gasifier: www.milenatechnology.com

OLGA tar removal: www.olgatechnology.com

SNG: www.bioSNG.com and www.bioCNG.com