



## **Allothermal gasification of biomass into chemicals and secondary energy carriers**

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**R.W.R. Zwart**

# Allothermal gasification of biomass into chemicals and secondary energy carriers

Robin Zwart



## Motivation for polygeneration

Make more  
money  
out of wood



↑  
High value product!

Increase the  
efficiency of  
wood conversion



## Motivation for polygeneration



↑  
Sales benefits?

↑  
High value product!

↑  
Production costs?

# Outline allothermal gasification towards chemicals and secondary energy carriers

- Motivation for polygeneration

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- Allothermal gasification: the MILENA at ECN
- Primary gas cleaning: the OLGA for tar removal

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- Possible secondary energy carriers
- Possible chemicals

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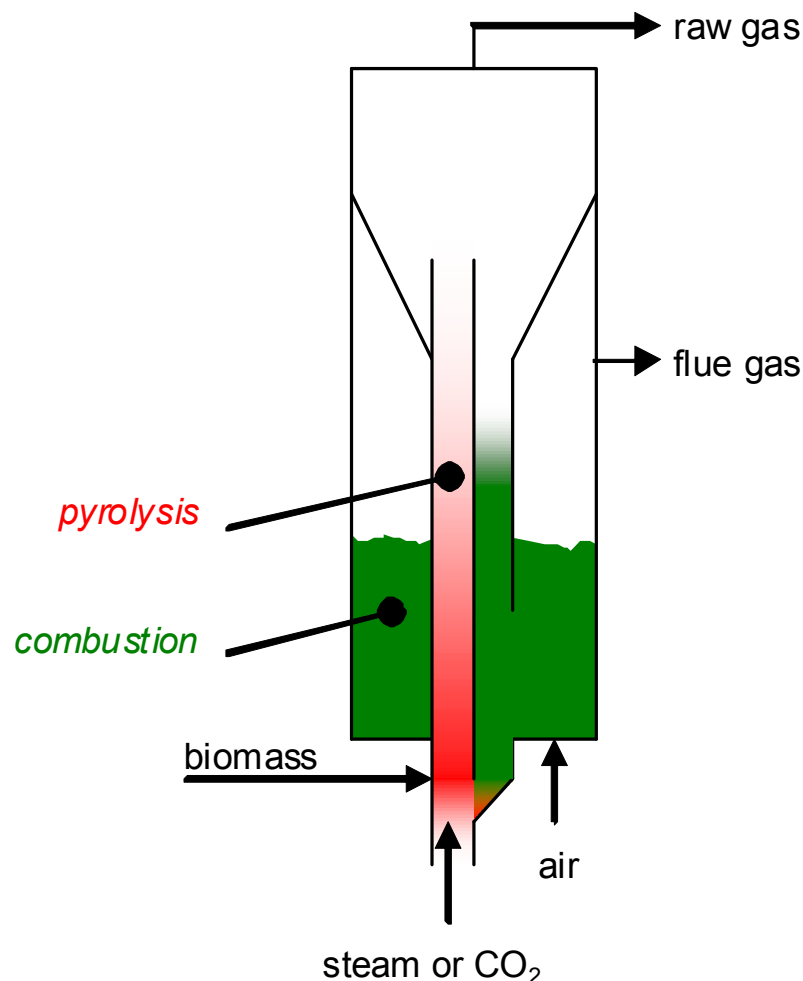
- Polygeneration concept and its feasibility

## Allothermal gasification: MILENA at ECN

- Low  $N_2$  in gas
- High methane yield
- Complete conversion
- Fuel flexible

### 160 kg/hr pilot plant:

- Riser diameter 0.2 m
- Combustor diameter 0.8 m
- Height 8.0 m

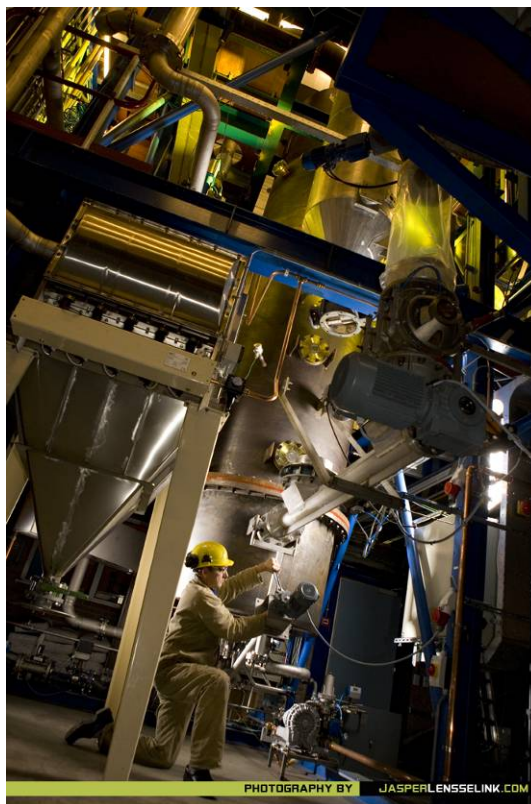




## Allothermal gasification: MILENA at ECN



25 kW



800 kW



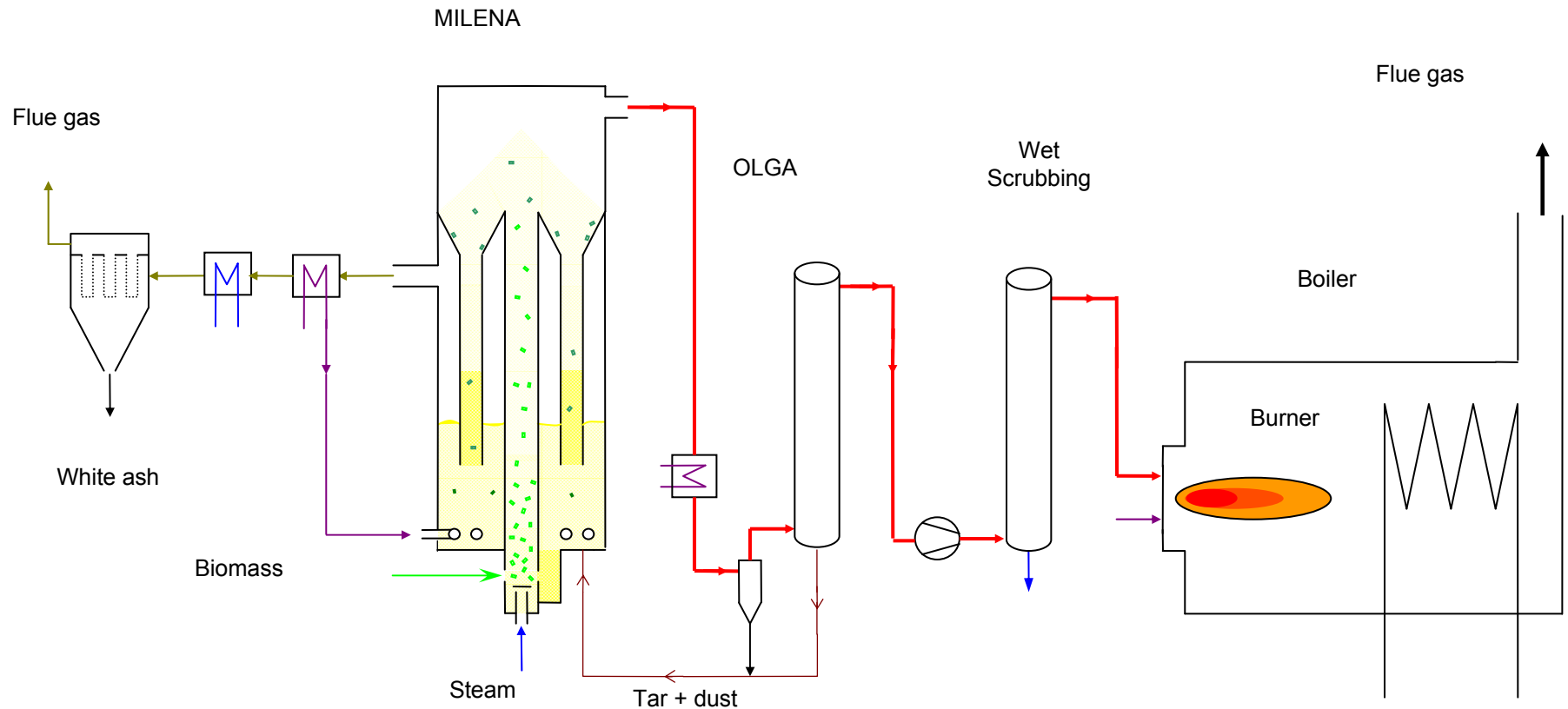
CHP  
10 MWth

scheduled for  
2012

SNG  
50 MWth

scheduled for  
2015

# Allothermal gasification: MILENA at ECN

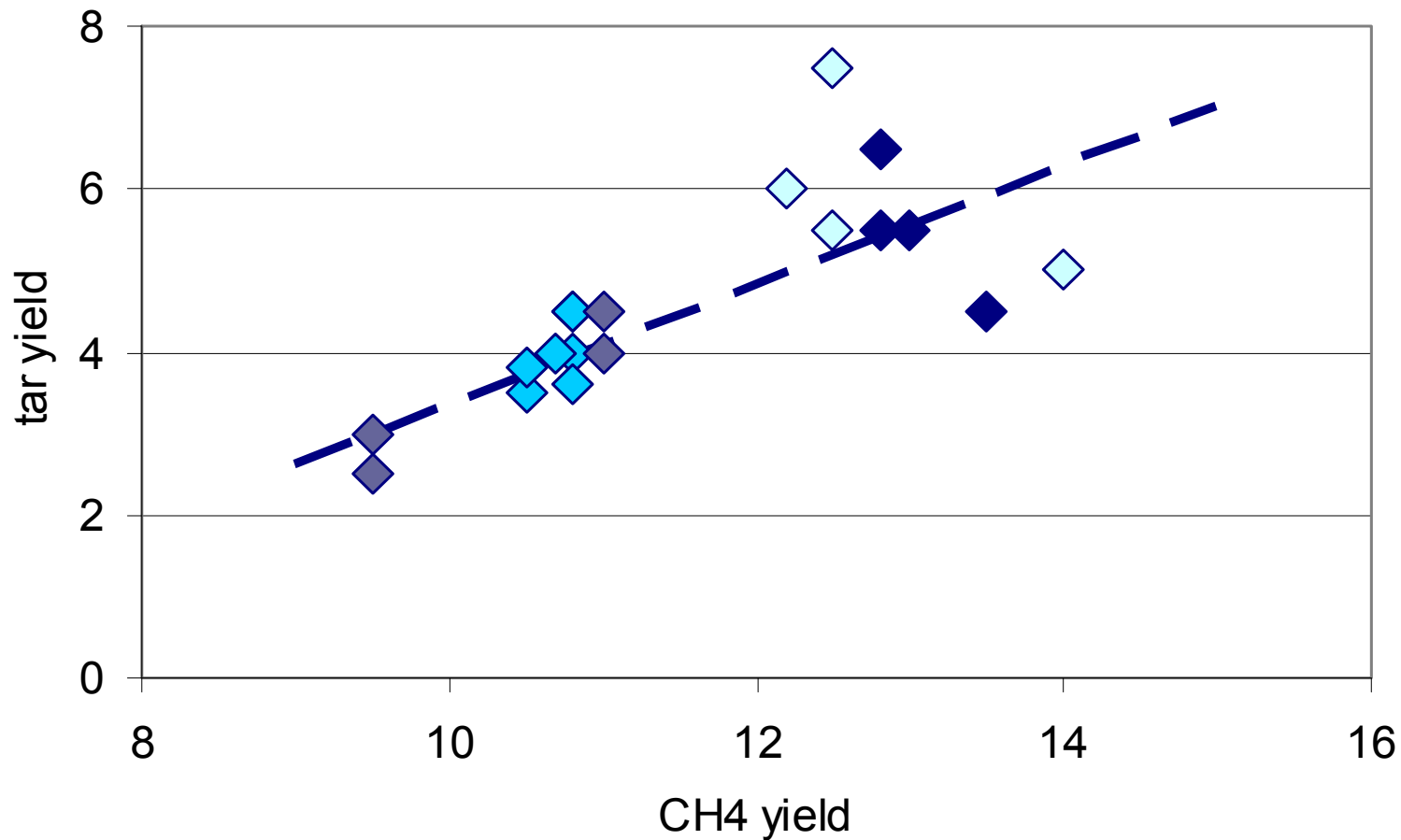




## Allothermal gasification: MILENA at ECN

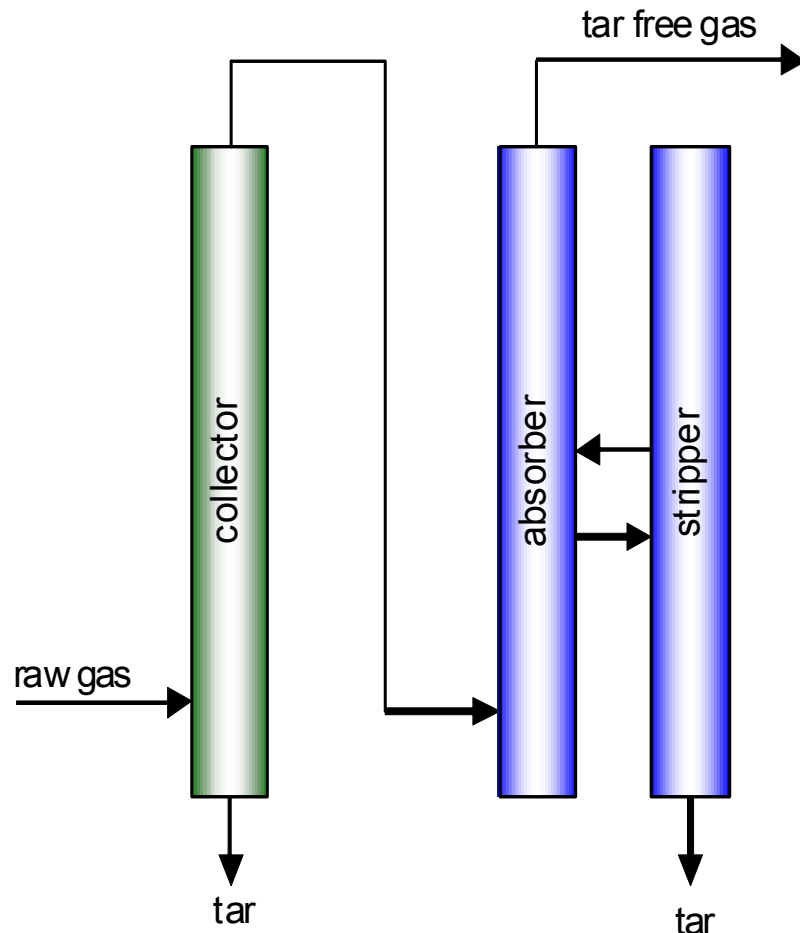
- Approximately 15 tests done, initially directly to the boiler.
- Fuel: wood pellets, throughput 120 and 150 kg/h
- Fluidization agent gasifier: steam (15 kg/h) or air (20 m<sub>n</sub><sup>3</sup>/h)
- Bed material -> Sand
- Estimated circulation rate bed material 3000 kg/h (design 6000). Circulation rate can be increased during testing
- Gas composition similar to lab-scale installation (tar content approx. 40 gram/m<sub>n</sub><sup>3</sup>)
- Issues to be solved:
  - Tar removal required (OLGA), tar condensation in front of burner, OLGA will be ready in **August**.
  - Sand causes friction problems between refractory wall and metal insert, modifications required.

## Allothermal gasification: MILENA at ECN



## Primary gas cleaning: OLGA for tar removal

- Complete tar removal
- No methane reduction
- Tar recycle to gasifier
- No water condensation
- Fits many types of gasifiers
- Creates freedom for gasifier optimization ...

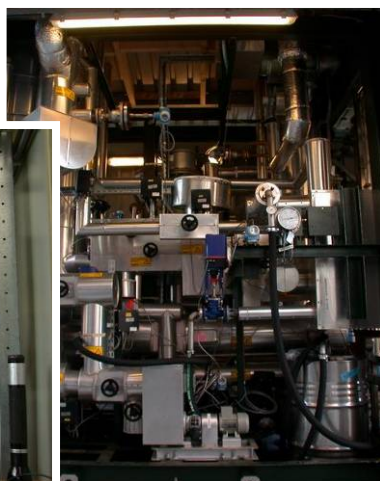


# Primary gas cleaning: OLGA for tar removal

**DAHLMAN**  
FILTER TECHNOLOGY



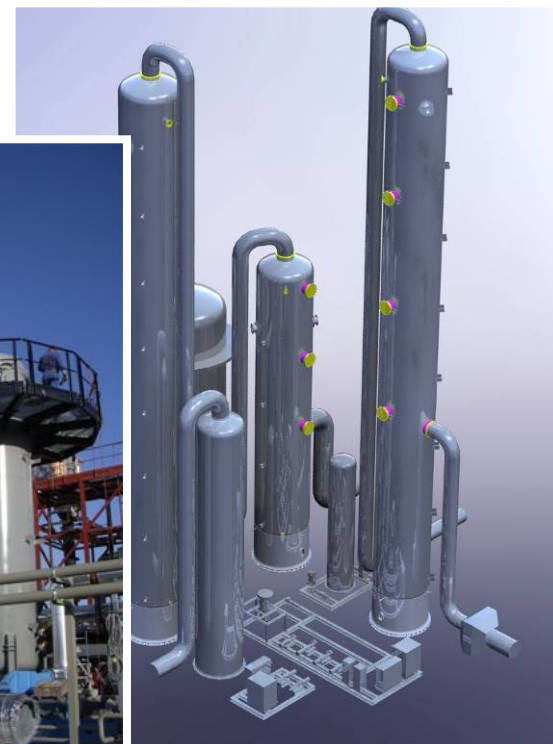
$2 \text{ m}^3/\text{h}$



$200 \text{ m}^3/\text{h}$



$2\,000 \text{ m}^3/\text{h}$



$25\,000 \text{ m}^3/\text{h}$

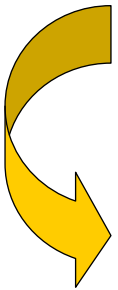


## Primary gas cleaning: OLGA for tar removal

Component		Downstream MILENA	Downstream OLGA
CO	vol%	30.1	30.6
H <sub>2</sub>	vol%	32.0	32.5
CO <sub>2</sub>	vol%	19.2	19.4
O <sub>2</sub>	vol%	0.0	0.0
CH <sub>4</sub>	vol%	12.2	12.4
N <sub>2</sub> +Ar	vol%	0.1	0.1
C <sub>2</sub> H <sub>2</sub>	vol%	0.2	0.2
C <sub>2</sub> H <sub>4</sub>	vol%	3.9	3.9
C <sub>2</sub> H <sub>6</sub>	vol%	0.2	0.2
C <sub>6</sub> H <sub>6</sub>	vol%	1.0	0.5
C <sub>7</sub> H <sub>8</sub>	vol%	0.1	0.0
Tar	g/mn <sup>3</sup>	52.1	0.2

## Possible secondary energy carriers

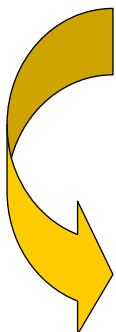
- Standard quality substitute natural gas ( $\text{CH}_4$ )
  - High quality substitute natural gas ( $\text{CH}_4$ ,  $\text{C}_2\text{H}_6$ , ...)
- 
- C1 chemistry based fuels ( $\text{CO} + \text{H}_2 \rightarrow \text{FT diesel, DME, ...}$ )
  - “The ultimate fuel” ( $\text{H}_2$ )
- 
- Heat
  - Power



All will depend on the scale of operation!

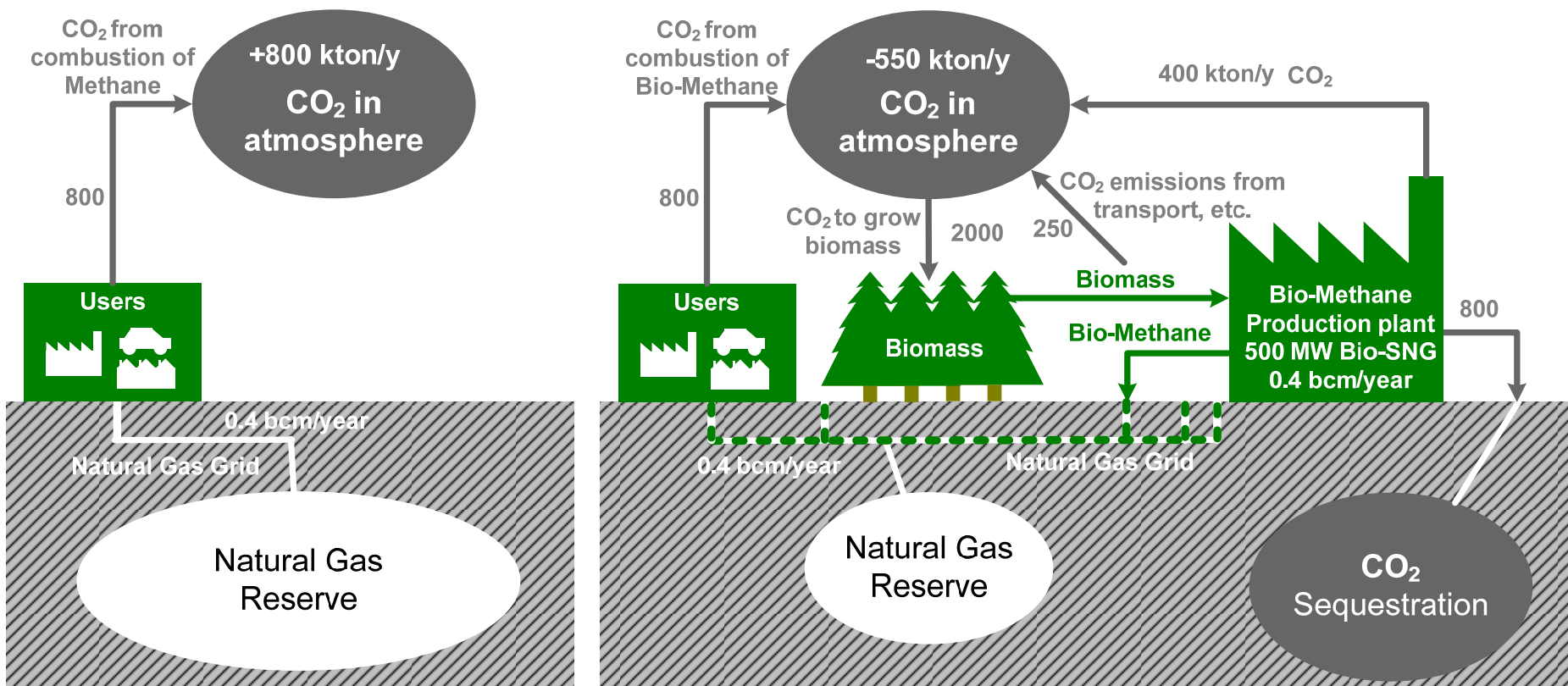
## Possible chemicals

- Acetylene ( $C_2H_2$  for bulk chemistry)
  - Ethylene ( $C_2H_4$  for bulk chemistry)
- 
- Benzene ( $C_6H_6$  for bulk chemistry)
  - Toluene ( $C_7H_8$  for bulk chemistry)
- 
- Carbon dioxide ( $CO_2$  for greenhouses)



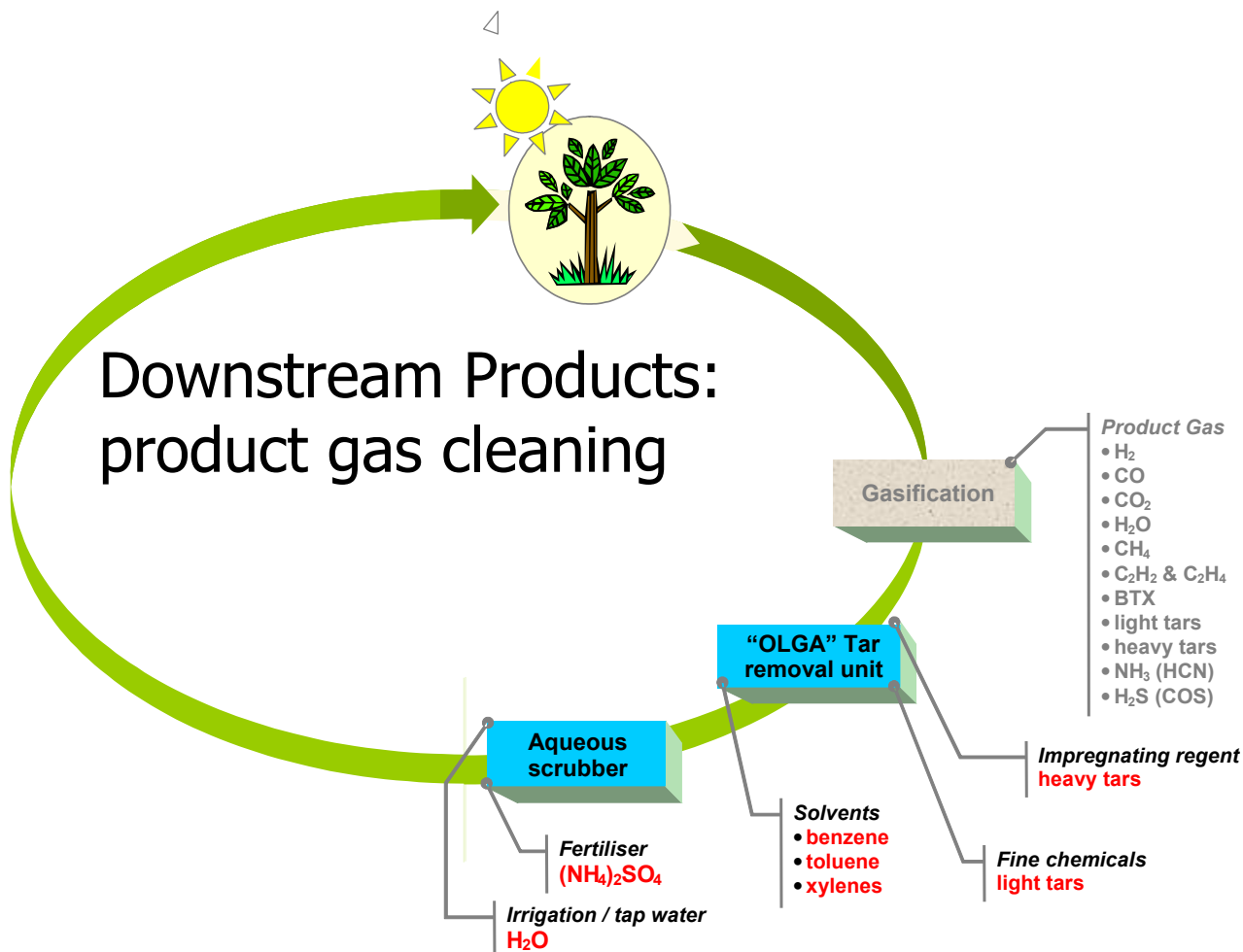
In many systems including a synthesis step,  $CO_2$  removal is implemented for volume reduction or product quality control!

## Possible chemicals

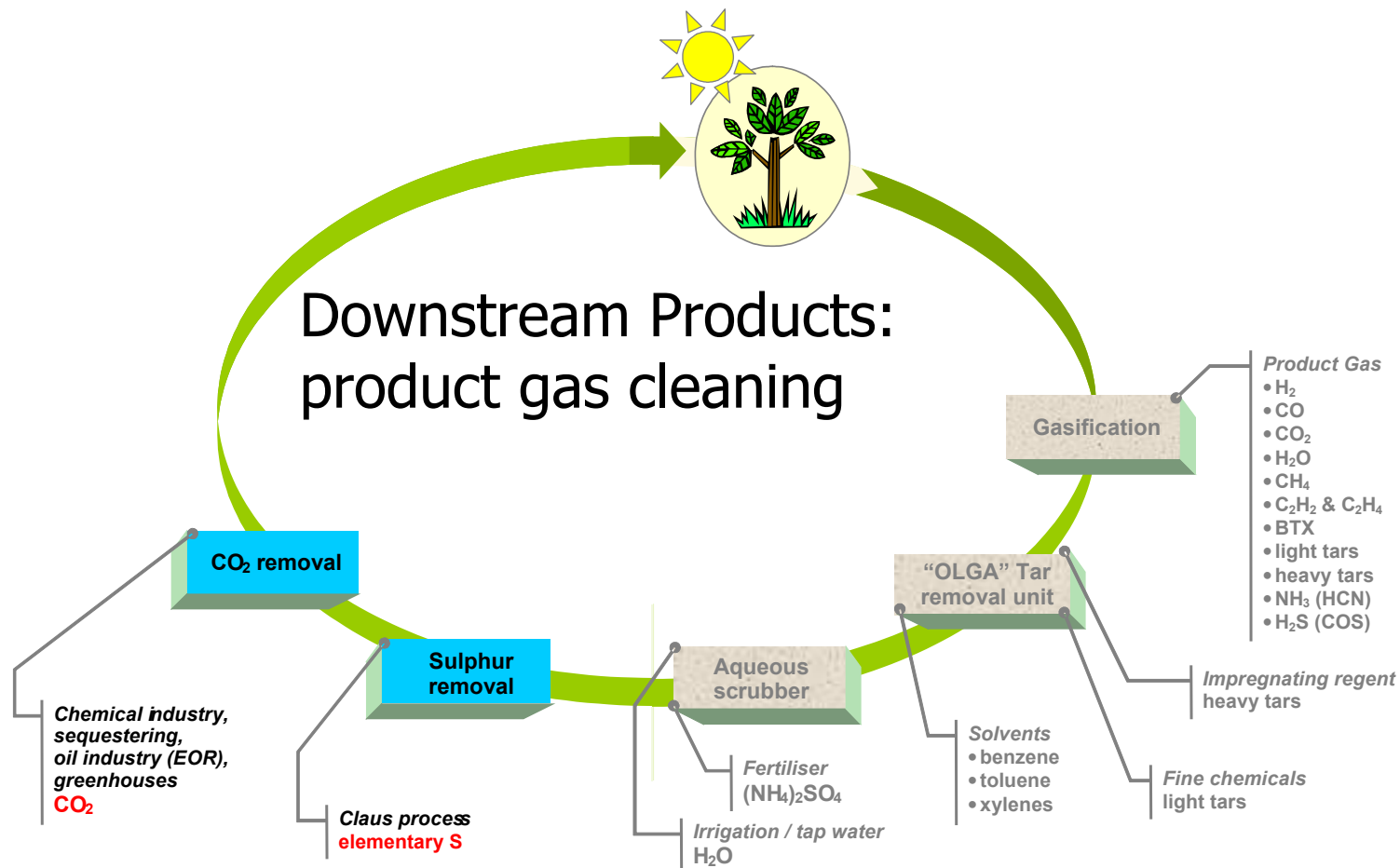




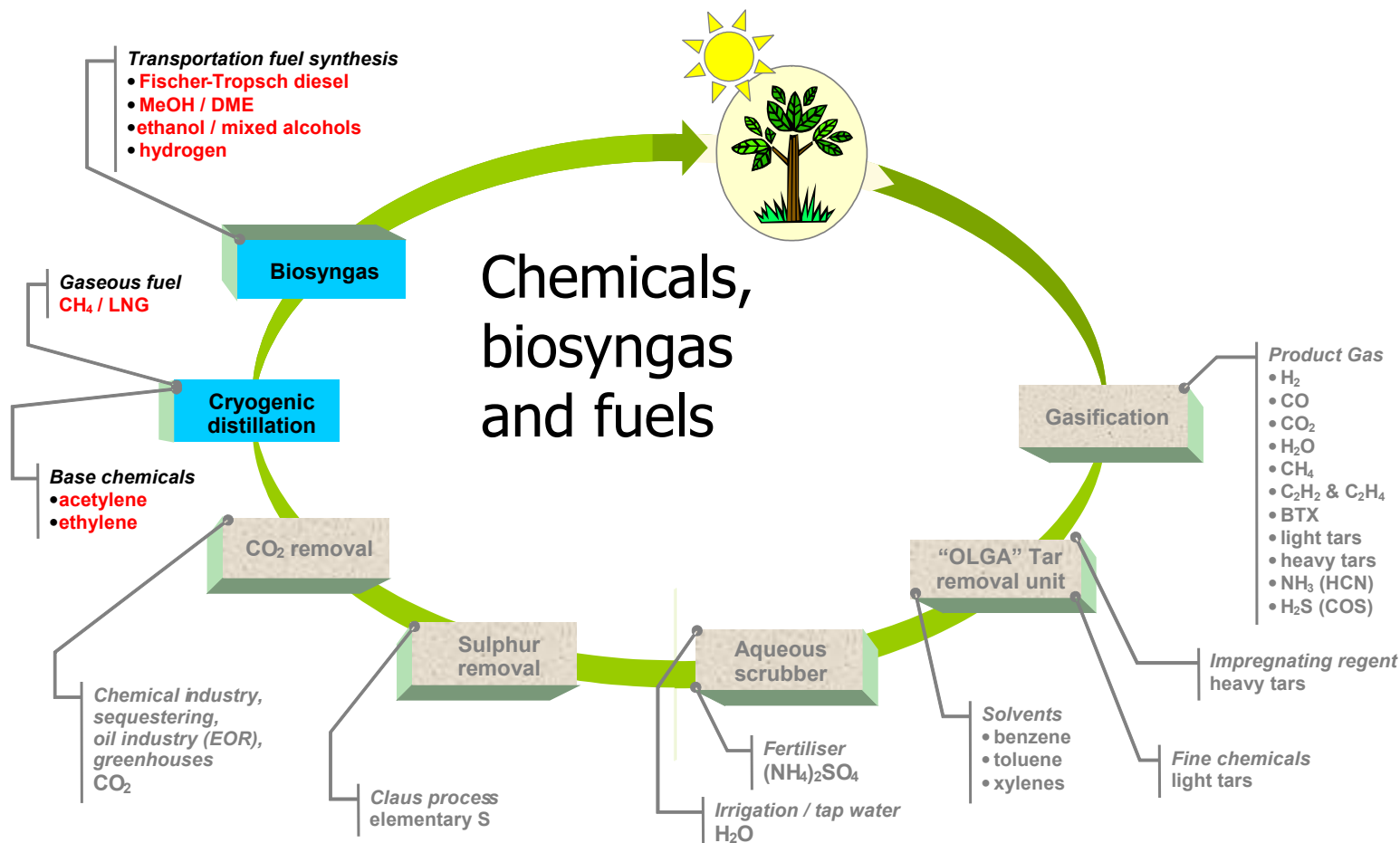
# Polygeneration concept



# Polygeneration concept

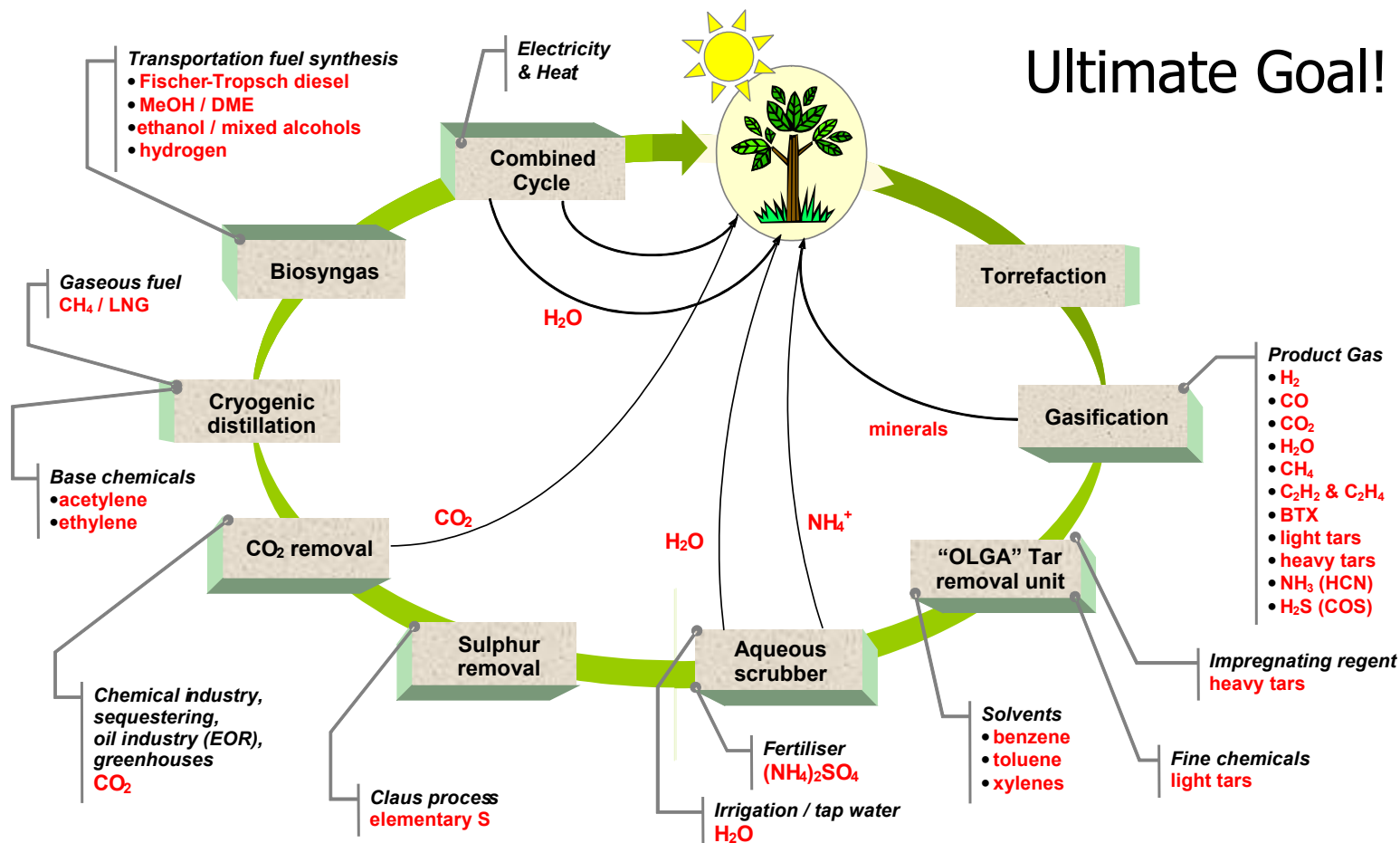


# Polygeneration concept



# Polygeneration concept

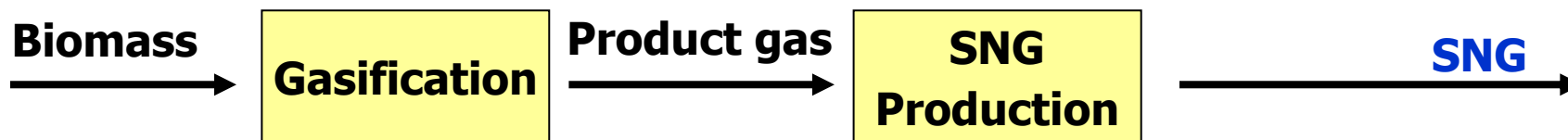
Ultimate Goal!



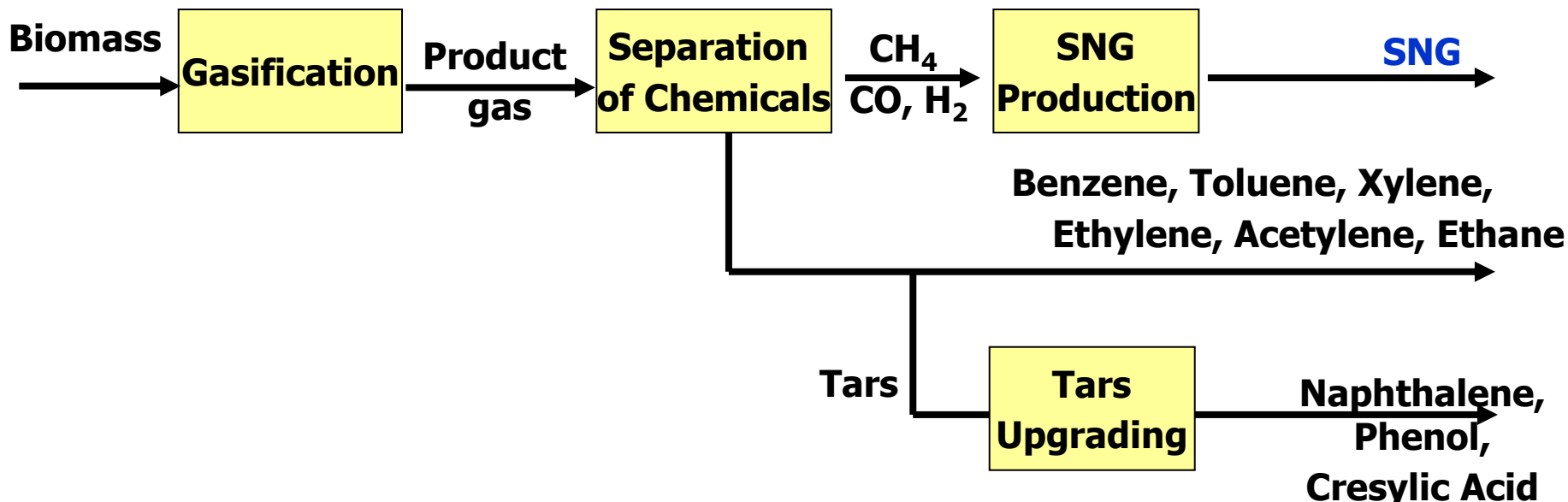


## Feasibility

### 1. Base Case : SNG Production via low temperature gasification

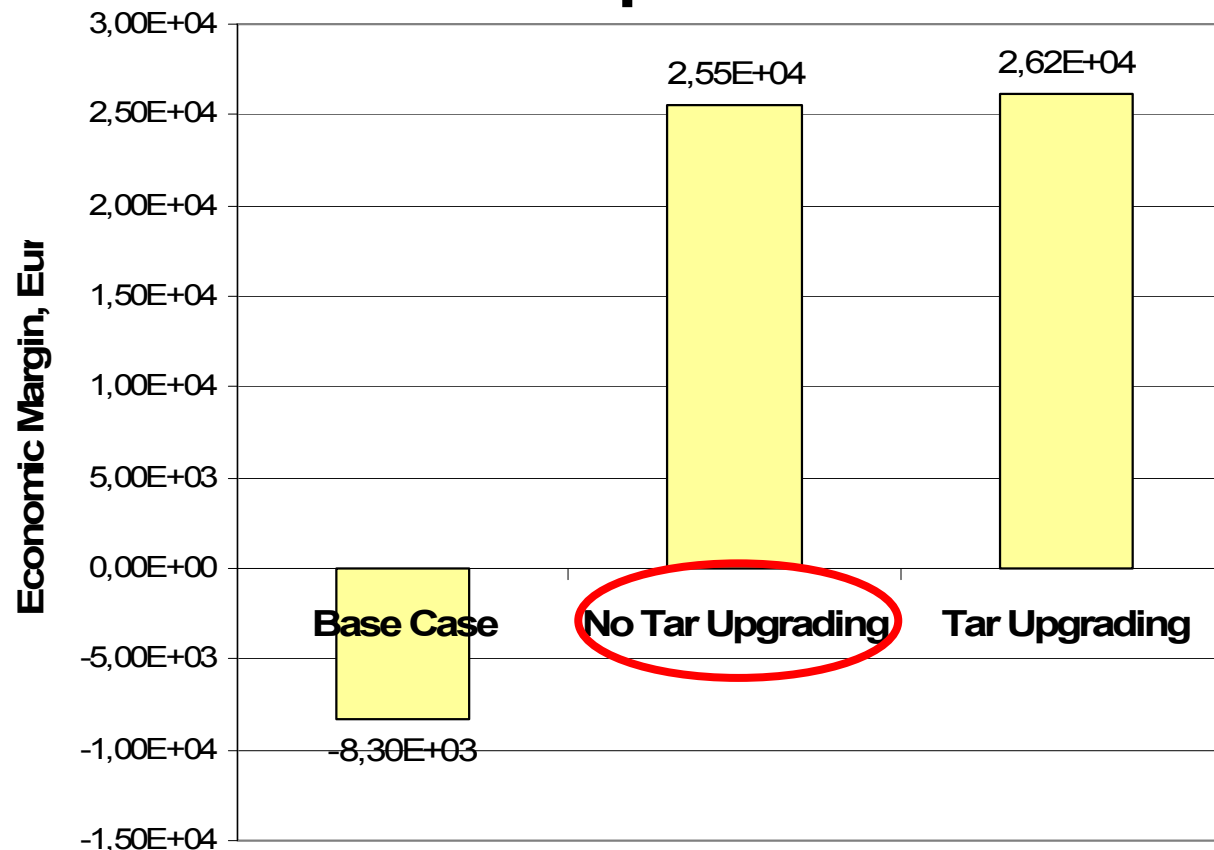


### 2. Separation of Chemicals



# Feasibility

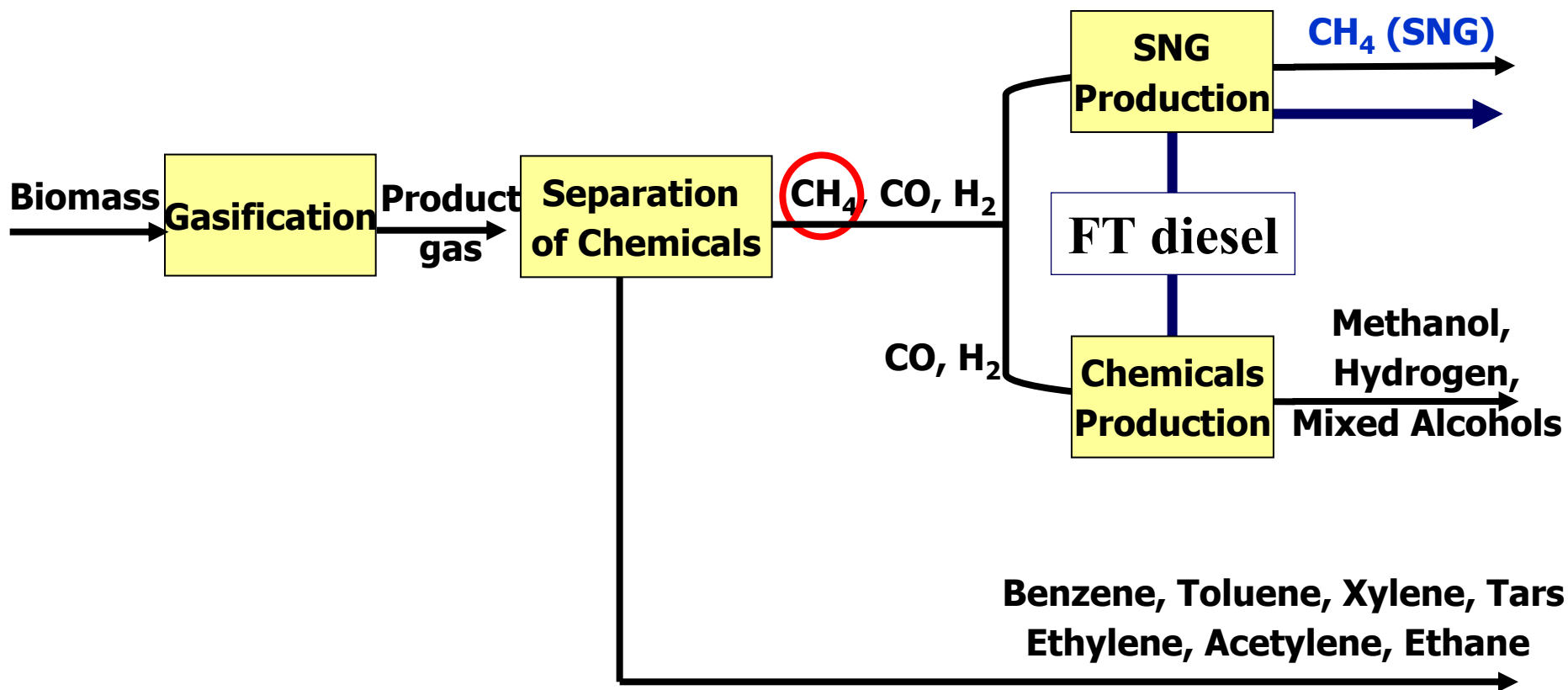
## Comparison



**Economic Margin = Sales Revenues – Raw Materials (Biomass)**  
 (on the basis of 100 kg/hr input of biomass)

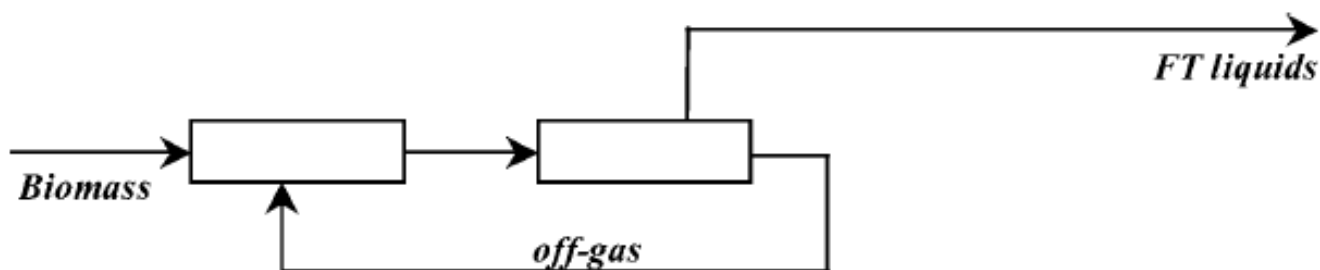
# Feasibility

## 3. Separation of Chemicals and Catalytic production of Chemicals

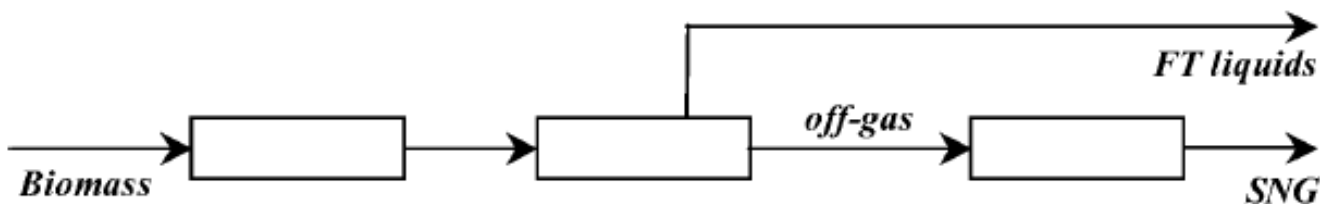


## Feasibility

592 *Energy & Fuels*, Vol. 19, No. 2, 2005

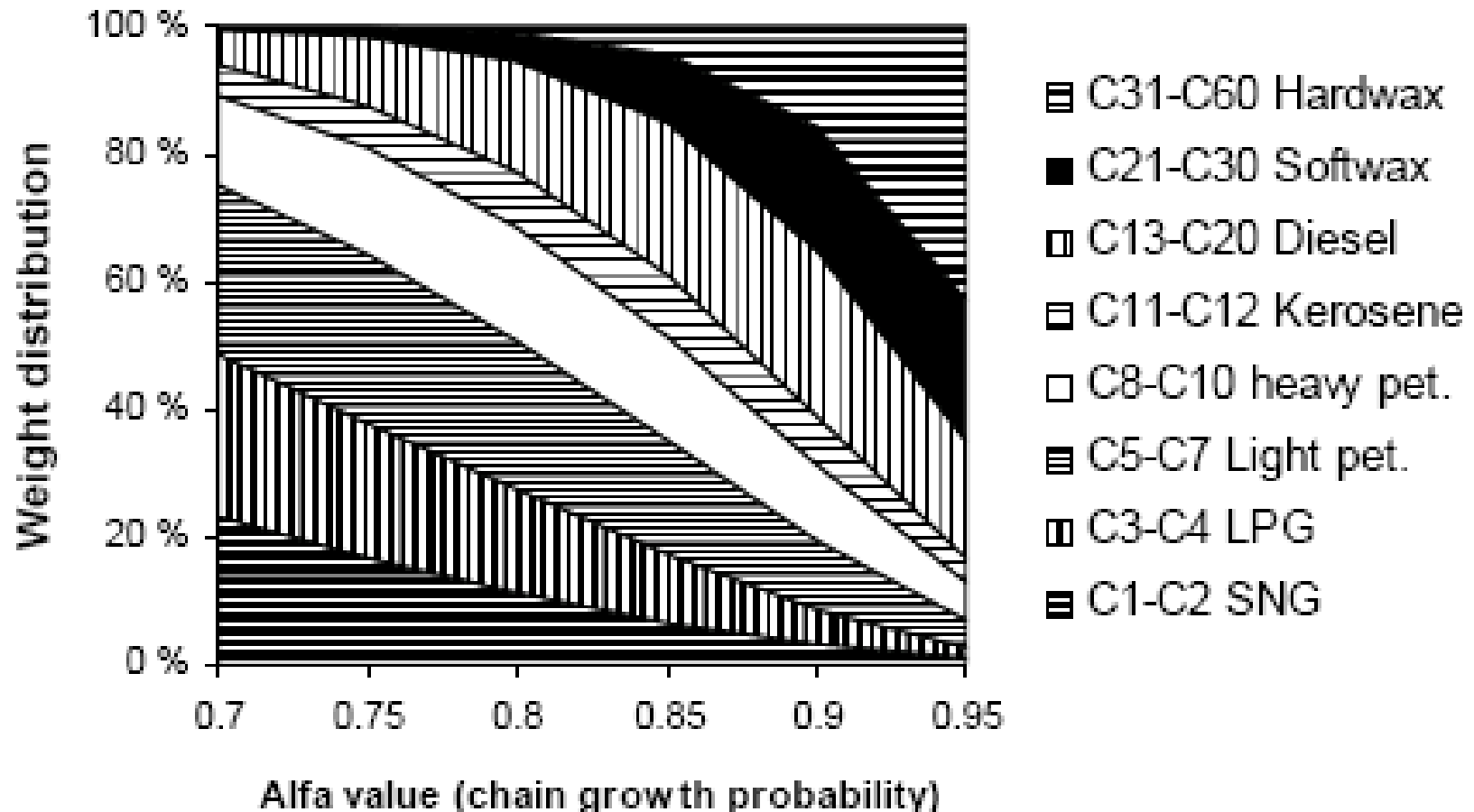


**Figure 1.** System for the production of Fischer–Tropsch (FT) liquids from biomass.



**Figure 2.** System for the co-generation of liquid FT transportation fuels and synthetic natural gas (SNG) from biomass.

## Feasibility



## Conclusion

- Polygeneration can be more than co-producing heat/power
- Chemicals can create additional economic margin...  
... though will require significant additional costs
- Fuels can create additional economic margin...  
... and might require less additional costs than thought
- Why work on allothermal gasification and C1 chemistry...  
... when your product gas contains all the interesting stuff?



## Contact information

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fuel composition database: [www.phyllis.nl](http://www.phyllis.nl)

tar dew point calculator: [www.thersites.nl](http://www.thersites.nl)

IEA bioenergy/gasification: [www.ieatask33.org](http://www.ieatask33.org)

Milena indirect gasifier: [www.milenatechnology.com](http://www.milenatechnology.com)

OLGA tar removal: [www.olgatechnology.com](http://www.olgatechnology.com)

SNG: [www.bioSNG.com](http://www.bioSNG.com) and [www.bioCNG.com](http://www.bioCNG.com)