



Organic-inorganic hybrid microporous membranes (HybSi®) for pervaporation applications

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ECN
Energy research Centre of the Netherlands

Organic-Inorganic Hybrid Microporous Membranes (HybSi®) for Pervaporation Applications

Jaap Vente

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ECN's location

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ECN's main features

- ECN develops high-level knowledge and technology for a sustainable energy management and transfers it to the market.
- Annual turnover of 70 million euro
- Approx. 5-10 international patents granted each year
- Approx. 600 reports and publications each year
- (Inter)national co-operation with companies, universities and research institutes

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Trias Energetica

1. Reduce demand (energy saving)
2. Maximise the use of renewable energy sources
3. Use fossil fuels in the cleanest possible way

Energy demand

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ECN's Structure

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graph TD
    Director["Director  
A.G.M. Hoff  
C.A.M. van der Klein"] --- PO["Personnel & Organisation  
J.H.P.C.A. Simons"]
    Director --- FF["Facilities and Finance  
G.P.J. den Hartogh, J.A.G. Stallinga"]
    PO --- Eng["Engineering & Service  
J. Saurwalt"]
    FF --- QSE["Quality, Safety & Environment  
J. Schrover"]
    Eng --- PS["Policy Studies  
J.R. Ybema"]
    Eng --- WE["Wind Energy  
T.J. de Lange"]
    Eng --- EI["Efficiency & Infrastructure  
P.T. Alderliesten"]
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F.A. de Brujin"]
    WE --- SE["Solar Energy  
P. Wyers"]
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J.W. Erisman"]
  
```

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Energy Efficiency in Industry

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Energy Efficiency in Industry

Industrial Heat Management
(10 fte)



Upgrading industrial waste heat
Thermo-acoustic heat pump
Chemical heat pump

Process Intensification
(7 fte)



Combined unit operations
Structured Membrane reactors
advanced distillation

Molecular Separation Technology
(13 fte)

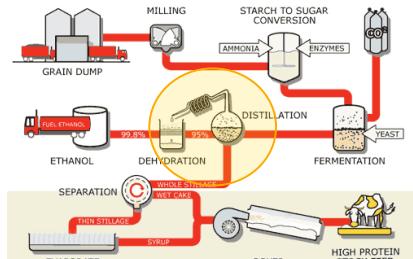


Molecular separations
Materials, processes
Systems development

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Bio-ethanol



The diagram illustrates the bio-ethanol production process. It starts with a grain dump, followed by milling. The milled grain undergoes starch to sugar conversion using enzymes and ammonia. The resulting sugar is fermented with yeast to produce ethanol. The ethanol is then dehydrated to 99.8% purity. The final step is separation, which yields thin stillage (95% water) and whole stillage (95% ethanol). The whole stillage is further processed through evaporation and a dryer to produce high protein stock feed.

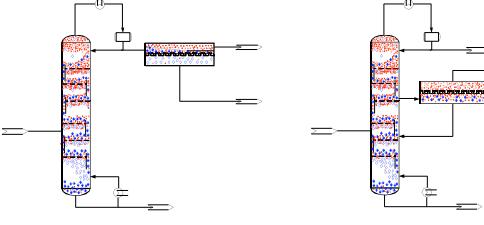
Source: www.miningnews.net

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Distillation – Membrane Integration



The diagrams show two configurations for distillation-membrane integration. The left diagram shows a distillation column with a membrane section for azeotropic separation. The right diagram shows a distillation column with a membrane section for debottlenecking, including a recycle stream.

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Pervaporation membranes

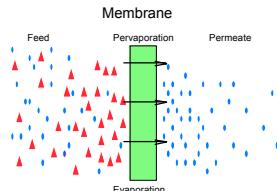
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What is pervaporation

Pervaporation is a membrane based separation technique

- = permeation + evaporation
- = selective evaporation of liquids via a membrane
- = much more energy efficient than distillation



The diagram illustrates the pervaporation process. A green vertical cylinder represents the membrane. On the left, red triangles represent the 'Feed' entering the membrane. On the right, blue triangles represent the 'Permeate' exiting the membrane. Below the membrane, blue triangles represent 'Evaporation' occurring within the membrane structure.

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External Developments

- Sulzer:**
PVA based membranes
 - Market leader
 - Well established
- Vaperma:**
Polyimide bases
 - Recently started
 - Large demonstrations
- Mitsui, Mitsubishi, Inocermic, Hyflux, Hitachi Zeolite A**
 - Various stages of commercialisation
 - Most widely used inorganic PV membrane

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Siftek™ Membrane by Vaperma

- Hydrophilic polyimide hollow fiber concept
- Vapour permeation from the bore side
- 100m² membrane area per module

Source  [vaperma](http://www.vaperma.com)

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Zeolite A membrane

Year	Separation factor, α	Permeation flux, $\text{kg m}^{-2} \text{h}^{-1}$
1997	~10 ⁴	~2
2000	~10 ⁴	~3
2007	~10 ⁴	~4
2008	~10 ⁴	~6

Pervaporation 75°C
Source 

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Applications

Main benefits expected:

- Azeotrope separations
 - (bio)-ethanol / water
 - acetonitrile / water
 - toluene / methanol
- Difficult distillations / close boilers
 - Acetic acid / water
 - Acetone / water
- Various recycle streams
 - NMP / water
 - DMF / water
- End of pipe (by)-product upgrading

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Present challenges

- Higher application temperatures
- Higher acid resistance
- Higher stability in aggressive solvents
- Resistance against contact with liquids (i.e. pervaporation vs vapour permeation)
- Larger application window w.r.t. water content
- Effective methanol removal

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Amorphous inorganic microporous networks

- SiO_2
- Methylated SiO_2
- Ti/ZrO_2
- HybSiP: SiO_2 with organic bridges

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Preparation: Sol Gel

Hydrophilic: $\text{RO-Si(OR)}_3 \xrightarrow[\text{H}^+]{\text{H}_2\text{O}} \text{RO}-\text{Si(OH)}-\text{O}-\text{Si(OH)}-\text{O}-\text{Si(OH)}-\text{OR}$

Hydrophobic: $\text{CH}_3-\text{Si(OR)}_3 \xrightarrow[\text{H}^+]{\text{H}_2\text{O}} \text{CH}_3-\text{Si(OH)}-\text{O}-\text{Si(CH}_3)-\text{O}-\text{Si(OH)}-\text{CH}_3$

TEOS: Tetraethylorthosilicate, MTES: Methyltriethoxysilane

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Membrane fabrication

coat speed
"dry"
"wet"
evaporation
coat vessel
septum
suspension

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Large scale production

Coat robot
Drying Carousel
Welding robot
Module
Furnace

Sulzer Chemtech

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$\text{SiO}_2 - \text{Me-SiO}_2$ pervaporation results (95°C)

• 5 wt.% H_2O in BuOH, 10 mbar
• Addition of MTES gives better performance with time
• Constant performance possible for over 18 months!

Chem. Comm. 2004, 834-835

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Me-SiO₂ pervaporation up to 165°C

2.5 wt.% H_2O in BuOH, 10 mbar
Failure within weeks
No clear relation with temperature

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ZrO_2 membranes

- Tuning of
 - Sol recipe
 - Concentration
 - Coating speed

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